

STANDARD OPERATING PROCEDURES

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Policy Number: SSMP 1-01

Effective Date: 9/03

STANDARD OPERATING PROCEDURE (SOP'S): DEVELOPMENT OF SOP'S

I. PURPOSE

To provide an effective way for developing and implementing Standard Operating Procedures (SOP's) for Norlite Corporation's plant operations and systems.

II. SCOPE

All Norlite Corporation Employees and Contractors.

III. RESONSIBILITIES

- A. The plant manager is responsible for approving all SOP's.
- B. The department managers and supervisors are responsible for developing and implementing the SOP's.
- C. Employees are responsible for following the SOP's.

III. PROCEDURES

GENERAL

SOP's are used as a means of communicating a written standard for each specific job function for any system or operation. SOP's should be developed in a way that effectively offers the employees a compliant, productive and safe means of operation.

The development of SOP's should be done in the following manner:

- 1. Identify the task or job function that needs to be performed.
- 2. Select responsible individual(s) to prepare the SOP.
- 3. Gather input from managers, supervisors and field personnel that will be involved in performing the task.
- 4. Analyze task for environmental, operational and safety issues.
- 5. Prepare a list of criteria from start to finish that must be followed to complete task.
- 6. Organize criteria and comments into concise steps that will accomplish task.
- 7. Review criteria and receive additional comments from personnel.
- 8. Prepare SOP as a SOP document. (see Attachment A as example of SOP layout)
- 9. Submit SOP for approval to next level of management.
- 10. After approval, incorporate SOP into operating manuals and train effected employees.



Policy Number: SSMP 1-02

Effective Date: 9/03 Revision Dates:

DOCUMENT CONTROL LOG (DCL) DOCUMENT CONTROL FILE (DCF)

I. PURPOSE

A system to track and manage data associated with projects, periodicals, permits and library reports.

II. SCOPE

All Norlite Corporation employees.

III. RESONSIBILITIES

All persons filing and/or retrieving data from the DCL and DCF.

PROCEDURES

- 1. Determine whether you have a Project, Periodical, Permit, or a Library Report.
 - a. A **Project** is a task that involves an exchange of information, which has an expected conclusion date (end date). Project numbers will begin with 2000 and continue in sequence.
 - b. A **Periodical** is an on going exchange of information, such as quarterly reports, manifest inquiries, or annual reports. Periodicals will be numbered in the 1000 series.
 - c. A **Permit** is a written warrant or license granted by one having authority which includes information such as permit application, renewals, and modifications. Permit numbers will begin with 3000 and continue in sequence.
 - d. A **Library Report** is a bound report. Library reports will be labeled as a volume and will begin with 100 and continue in sequence.
- 2. When submitting documents for either a project, periodical, or a permit DCL Number, you must provide the following information:
 - a. Project Title
 - b. Whether the information is in-coming, out-going or internal.
 - c. Initiation date
 - d. Point of Contact (POC) individual
 - e. Any notes or comments
- 3. When adding bound reports to the library for a Volume Number, you must Provide the following information:

Policy Number: SSMP 1-02 **DOCUMENT CONTROL LOG (DCL) DOCUMENT CONTROL FILE (DCF)**

- a. Report Title
- b. Whether report is in-coming, out-going, or internal
- c. Date of report
- d. Point of Contact (POC) individual
- e. Notes or comments

Projects:

- 1. Acquire a Project Number from the Compliance Administrative Assistant and remit all original documents to be filed in the DCF.
- 2. All documents such as letters, telephone logs, faxes, electronic mail and reports will have a Document ID. As documents are received and generated, they will promptly be remitted to the DCF, and working copies are to be made as necessary. Telephone logs can be obtained from the DCL or electronically from the Compliance Administrative Assistant.
- 3. The Document ID will consist of the Project Number followed by a letter in alphabetical sequence (i.e. 2000a, 2000b). The Document ID Number must be clearly marked on the corresponding document

Periodicals:

- 1. Acquire a Periodical Number from the Compliance Administrative Assistant.
- 2. Each completed report (i.e. monthly, quarterly, yearly) will receive a Document ID Number.
- 3. The Document ID will consist of the Periodical Number followed by a letter in alphabetical sequence (i.e. 1000a, 1000b). The Document ID must be clearly marked on the corresponding document.
- 4. In the event additional information regarding a periodical is requested, the Point of Contact (POC) individual will need to determine:
 - a. To include the supporting documentation with the existing periodical, and issue a Document ID $\,$ OR -
 - b. To create a new project by issuing a new Project Number.

Permits:

- 1. Acquire a Permit Number from the Compliance Administrative Assistant and remit all original Permit documents to be filed in the Permit Document file,
- 2. All official documents will have a Document ID. As documents are received and generated, they will promptly be remitted to the document file, and working copies are to be made as necessary.
- 3. The Document ID will consist of the Permit Number followed by a letter in alphabetical sequence (i.e. 3000a, 3000b). The Document ID Number must be clearly marked on the corresponding document.

Policy Number: SSMP 1-02

DOCUMENT CONTROL LOG (DCL) DOCUMENT CONTROL FILE (DCF)

Library:

1. Acquire a volume Number from the Compliance Administrative Assistant and remit all original reports to be added to the "Bookshelf."

2. The Bound Report ID will consist of the Volume Number followed by a Copy Number (i.e. 100 copy: 1 of 2, 100 copy: 2 of 2). The Report will be documented in the Library section of the DCL book for easy reference.

File Management:

- 1. The DCL, along with the active projects, permits, and appropriate periodicals, will be stored in the file cabinet labeled "Document Control File" in the Compliance Department and maintained by the Compliance Administrative Assistant.
- 2. All active projects will be filed in the DCF cabinet. Once a project is concluded the Point of Contact (POC) individual will determine whether the project will remain on site for one year (1yr), three years (3yr) or life of facility (LOF).
- 3. Periodicals that are ongoing will be the responsibility of the Point of Contact (POC) individual, unless other wise stated. It will be the POC individual's responsibility to update the DCL and the Document ID Summary.
- 4. Original Permits will be filed in the Permit Document Control File cabinet.
- 5. Projects/ periodicals can be stored as one year (1yr), three year (3yr), or life of facility (LOF).
 - a. One Year (1yr): **Projects**: will be stored in the Compliance Department. **Periodicals**: will be stored either with the POC individual or in the Compliance Department. See DCL for location of file.
 - b. Three Years (3yr) or Life of Facility (LOF): Projects/ Periodicals: may be stored in the Compliance Department or in the on-site Compliance storage trailer. Periodicals may also be with the POC individual. See DCL for location of all Files.
 - i. It is up to the discretion of the POC individual to determine whether the projects/ periodicals will be stored in the Compliance storage trailer. When files are stored in the Compliance storage trailer they will be stored in File Safe boxes with File Safe storage tracking numbers on them. The Front Desk Receptionist will issue File Safe tracking numbers.
- 6. **Projects/ Periodicals** requiring off site storage will be boxed in File Safe boxes and given a File Safe storage tracking number. The Front Desk Receptionist will issue File Safe tracking numbers.
 - a. Off-Site: All off-site storage will be held at File Safe Record Management, 12 Arrowhead Lane, Cohoes, NY 12047. All tracking numbers will be clearly

Policy Number: SSMP 1-02

DOCUMENT CONTROL LOG (DCL) DOCUMENT CONTROL FILE (DCF)

indicated in the DCL as will as on the File Safe "Norlite Data Storage Inventory" log located at the Front Desk Receptionist.



Policy Number: XXXXX Effective Date: XXXX

SOP TITLE

I. PURPOSE

Provide summary identifying the objective of the SOP.

II. SCOPE

Provide area or employees that are to be affected.

III. RESONSIBILITIES

List responsible personnel or departments. May be more than one.

III. PROCEDURES

Provide list of criteria (in order of completion) to be followed for performing particular task.



Policy Number: SSMP 1-03

Effective Date: 9/03

MACT REGULATORY CONTACT AND REPORTING

I. PURPOSE

Provide a basis for the MACT regulatory reporting requirements and whom to report to.

II. SCOPE

LWAK and APC

III. RESONSIBILITIES

Operations and Environmental Management Staff

IV. PROCEDURES

Regulatory Reporting Requirments

- 1. **Semi-Annual SSM Reports** sent to the regulatory agencies and includes the following:
 - events that did not follow the SSMP
 - excessive exceedance reports
 - summary report of all times of startup, shutdown or malfunction
- 2. **Excessive Exceedance Reports**-report is filed with agencies if there are 10 or more exceedances in a 60-day period.
 - Must submit written report of the 10 exceedances within 5 days of the 10th exceedance.
- 3. **Immediate SSMP Reports**-report must be filed if actions taken during an SSM event are not consistent with SSMP or written SOP's.
 - Must verbally notify the agency within 2 days of event and must follow up with letter with in 7 days.
 - Must update SSMP and/or SOP's that have been deviated from or not been established within 45 days of deviation.

Who to report to: make report to both agencies listed below.

NYSDEC

Attn: Parag Amin Central Office 625 Broadway Albany, NY 12233

Tel: (518) 402-8609

USEPA

Attn: Kenneth Eng

Air Compliance Branch-Region 2

290 Broadway

New York, NY 10007-1866

Tel: (212) 637-4069



Policy Number: SSMP 2-01

Effective Date: 9/03

KILN STARTUP PROCEDURE-COLD

I. PURPOSE

Provide a compliant, efficient and safe means of startup for the Lightweight Aggregate Kilns (LWAK) and associated Air Pollution Control Equipment (APC) from a cold* state of operation.

II. SCOPE

LWAK and APC

III. RESONSIBILITIES

Kiln Burner Operators and Kiln Supervisors.

IV. PROCEDURES

- 1. Pre-Heat Up.
 - a. Open make-up water to fill recycle tank.
 - b. Start recycle pump, establish flow.

2. Heat-Up: 1st Stage. Cold to 600°F

- a. Establish air flow to Pilot, Fire eye.
- b. Turn gas/fuel oil pilot switch on.
- c. Ignite pilot.
- d. Turn main gas switch on.
 - i. Open/Reset semi-auto Maxon valves.
 - ii. Turn main gas on (1-2 lines).
 - 1. Time frame between Pilot and Main gas may depend on weather and/or maintenance done.
- e. Open LGF vent valve.
- f. Open quench, mist pad and emergency water valves. Start quench pump.
- g. Establish caustic flow.
- h. Start blowdown pump. Establish flow.

At 200-300°F Backend temperature (mra).

- a. Start ID Fan at 30%.
- b. Increase ID Fan 10-15% and add one (1) line of gas approximately every hour.
- i. Begin rotating kiln on Pony Drive.

3. Heat-Up: 2nd Stage. 600-1100°F

- a. Start Primary Air fan.
- b. Continue adding one (1) line of gas and increasing fan 10-15% per hour.
- c. Start Heat Exchanger fans.
- d. Begin Lime Flow to baghouse.
- e. Start front Baron fan.
- f. Switch to waste oil, gas off.
- g. Switch kiln to main drive for continuous rotation.
- h. Start tire/nose ring fans.
- i. Start cooler system, conveyor.
- j. Start shale conveyors and introduce shale into kiln (12-14 tph) Once back-end temperature is between 1070-1100°F mra.
- k. Ensure all MACT/RCRA parameters are in spec, then switch to LGF.
- 1. Once clinker reaches cooler, turn on cooler fans.

the same and the



Policy Number: SSMP 2-02

Effective Date: 9/03

KILN STARTUP PROCEDURE-WARM

I. PURPOSE

Provide a compliant, efficient and safe means of startup for the Lightweight Aggregate Kilns (LWAK) and associated Air Pollution Control Equipment (APC) from a warm* state of operation.

II. SCOPE

LWAK and APC.

III. RESPONSIBILITIES

Kiln Burner Operators and Kiln Supervisors.

IV. PROCEDURES

WARM KILN STARTUP will follow the same procedures as COLD KILN STARTUP starting at a minimum of Step 2-e of the COLD KILN STARTUP procedure (SSMP 2-01).

"Depending on nature of repairs and/or length of time kiln has been down, some steps may have been already covered."

- 1. Re-heat kiln on Gas.
- 2. Adjust ID fan accordingly.
- 3. Re-start lime system if not already running.
- 4. At 600-800°F Back-end Temperature, continue with SSMP 2-01, step 3.

To ensure emissions are minimized, LGF cannot be turned on until kiln Back-end temperature exceeds 1020°F for one minute and shale has been introduced into the barrel.

It will be the operators/supervisors responsibility to determine what step he/she is at in the KILN WARMUP process and follow procedures accordingly.

Different Kiln temperatures will result in starting at different steps of the procedure.



Policy Number: SSMP 2-03

Effective Date: 9/03

KILN SHUTDOWN-PLANNED/ROUTINE

I. PURPOSE

Provide a compliant, efficient and safe means of a cold shutdown for the Lightweight Aggregate Kilns (LWAK) and associated Air Pollution Control Equipment (APC).

II. SCOPE

LWAK and APC

III. RESPONSIBILITIES

Kiln Burner Operators and Kiln Supervisors.

IV. PROCEDURES

- 1. Stop shale feed and turn conveyors off.
- 2. To minimize emissions, LGF flow should be stopped within 25 minutes from the time shale feed was cut-off, turn Low Grade Fuel (LGF) OFF and switch to Fossil Fuel.
- 3. After kiln is empty:
 - a. Close LGF vent valve.
 - b. Turn Fire/Pilot OFF.
 - c. Close LGF, Oil and Gas Valves.
 - d. Place N2 failsafe switch in OFF position.
 - e. Turn Gas/Pilot switch OFF.
 - f. Turn Lime system OFF for the appropriate kiln.
 - g. ID fan will remain ON for cool down of kiln, depending on planned entry time.
- 4. Continue to run APC equipment.
- 5. Run cooler until all material is discharged, then SHUTDOWN drive, screens, fans and conveyors and front Barron fan.
- 6. Turn off kiln drive. The Pony motor may be used to turn the kiln at a slower speed.
- 7. Shut OFF Heat Exchanger fans.
- 8. Shut OFF ID fan.
- 9. Shut Scrubber down:
 - a. Turn make-up water OFF.
 - b. Turn recycle pump OFF.
 - c. Turn caustic flow OFF, feed valves OFF, returns OPEN.
 - d. Continue blowdown until tank is EMPTY.
- 9. KILN rotation may be stopped as needed.



Policy Number: SSMP 2-03A

Effective Date: 9/03

KILN SHUTDOWN-EMERGENCY/UNEXPECTED

I. PURPOSE

Provide a compliant, efficient and safe means of an emergency/unexpected shutdown for the Lightweight Aggregate Kilns (LWAK) and associated Air Pollution Control Equipment (APC).

II. SCOPE

LWAK and APC

III. RESPONSIBILITIES

Kiln Burner Operators and Kiln Supervisors.

IV. PROCEDURES

Emergency/Unexpected kiln shutdown can occur at anytime. In order to minimize emissions, the following procedures should be followed at a minimum, if the situation for the shutdown allows.

- 1. Stop shale feed to Kiln.
 - a. Turn conveyors, rotary valve and accurate feeder off if necessary.
- 2. LGF or Fossil Fuel may be required to be shutoff immediately. If not;
- 3. LGF flow should be stopped within 25 minutes from the time shale feed was cut-off.
 - a. Cut the LGF flow and switch to fossil fuel (used oil or natural gas)
- 4. After kiln is empty:
 - a. Close LGF vent valve.
 - b. Flame Out (used oil or gas), Valves closed.
 - c. Primary Air fan OFF.
 - d. Pilot OFF/Switch OFF
 - e. Place N2 failsafe switch in OFF position.
 - f. Turn Lime feeder OFF.
 - i. If Shutdown does not require ID Fan to be shutdown, Lime rotary valve and blower may continue to run.
 - g. ID fan will remain ON for cool down of kiln, depending on planned entry time OR;
 - i. If entry is not required, ID Fan will remain on at a speed not to exceed maximum amperage.
 - ii. If entry is required; (if possible), the slow ramping down of fan speed should be used, so not to cause thermal shock of kiln.
- 5. Run cooler until all material is discharged, then SHUTDOWN drive, screens, fans and conveyors and front Barron fan.
 - a. If entry into cooler is not required, system may continue to run.

KILN SHUTDOWN-EMERGENCY/ UNEXPECTED

POLICY NUMBER: SSMP 2-03A

- 6. Continue to run APC equipment.
- 7. Shutdown both Heat Exchanger fans.
 - a. If entry is not required, fans may remain on to aid cool down.
- 8. Shutdown ID fan.
 - a. If entry is not required, fan will remain on.
- 9. Shutdown Scrubber.
 - -If entry is not required, scrubber will remain on (recycle, blowdown, caustic)
 - a. Turn make-up water/caustic off.
 - i. If shutdown does not require recycle tank to be empty, maintain tank level and caustic flow to ensure pH balanced water to wwtp.
 - ii. Otherwise close make-up water valve, close caustic feed valves and open returns.
 - b. Turn recycle pump off.
 - c. Turn quench pump off.
 - d. Close quench, mist pad, emergency water valves.
 - e. Turn blowdown pump off, after tank is empty.
- 10. Kiln rotation may be stopped as needed.



NORLITE CORPORATON
Policy Number: SSMP 2-04

Effective Date: 9/03

Revised: 10/03

MINIMUM KILN BACKEND TEMPERATURE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for exceeding the span limits or the minimum Kiln Backend Temperature of 866°F.

II. SCOPE

Minimum Kiln Backend Temperature

III. RESPONSIBILITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated for the Kiln Backend temperature.

- 1. Check for high Venturi and/or Ducon differential pressure (DP). (refer to SOP SSMP 3-03)
- 2. Check for high baghouse DP. (refer to SOP SSMP 3-02)
- 3. Check for loss of ID fan. (refer to SOP SSMP 2-18)
- 4. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result decreased kiln backend temperature.
- 5. Insure instrumentation measuring the Kiln Backend Temperature is operating correctly. Call I&E if there is a problem.



Policy Number: SSMP 2-05

Effective Date: 9/03 Revised: 10/03

MAXIMUM BAGHOUSE INLET TEMPERATURE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for exceeding the span limits or the maximum Baghouse Inlet Temperature of 400°F.

II. SCOPE

Baghouse Inlet Temperature

III. RESPONSIBILITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated for the Baghouse Inlet Temperature.

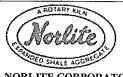
Loss of Heat Exchanger Fan -refer to SOP SSMP 3-01

Loss of ID Fan –refer to SOP SSMP 2-18

Loss of Dilution Damper –refer to SOP SSMP 2-19

<u>Instrumentation</u> - Insure instrumentation measuring the Kiln Backend Temperature is operating correctly. Call I&E if there is a problem.

To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the maximum baghouse inlet temperature.



Policy Number: SSMP 2-06

Effective Date: 9/03 Revised: 10/03 8/04

MAXIMUM STACK GAS FLOW RATE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for exceeding the span limits or the Maximum Stack Gas Flow Rate of 60,000 wscfm.

II. SCOPE

Stack Gas Flow Rate

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated for the Stack Gas Flow Rate.

- 1. Check the following components that could indicate restrictions at baghouse modules.
 - a. Baghouse DP-High
 - b. Venturi/Ducon DP-High
 - c. Heat Exchanger DP-High (tube restrictions)
 - d. Fan/Bearing failure
- 2. If problem persists, flame out/shut down and call I & E to check instrumentation failure.
- 3. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the maximum stack gas flow rate.



Policy Number: SSMP 2-07

Effective Date: 9/03 Revised: 10/03

MINIMUM VENTURI PRESSURE DROP

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the Venturi Pressure Drop to exceed the span limits or fall below the minimum of 2.0 inches water column (wc).

II. SCOPE

Venturi Pressure Drop

III. RESPONSIBIILITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated for the Venturi Pressure Drop.

- 1. Loss of ID fan –refer to SOP SSMP 2-18.
- 2. Baghouse Air Restriction
 - a. Adjust pulsers in MCC at PLC panel
 - -Turn both black needle dials counter clockwise past red needle. This will lower DP for baghouse. Do this for each module.
 - b. If DP does not lower or baghouse is not pulsing, check the following:
 - i. Check for air leaks on top of the baghouse at pulsing solenoid by shutting ball valve on leaking solenoid; cleaning of bags will resume.
 - c. Check Ducon DP (High DP)
 - i. Verify water flow to mist pad.
 - ii. Increase flow to mist pad to lower Ducon DP.
 - d. Verify operation of Heat Exchanger fans.
 - e. Verify operation of Dillution Damper.
 - f. Increase ID fan speed. (not to exceed 400 amps)
- 3. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the minimum venturi pressure drop.
- 4. Insure instrumentation that measures the pressure drop is operating correctly. Call I&E if problematic.

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Policy Number: SSMP 2-08

Effective Date: 9/03 Revised: 10/03

MINIMUM SCRUBBER BLOWDOWN RATE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the Scrubber Blowdown Rate to exceed the span limits or fall below the minimum of 13.0 gallons per minute (gpm).

II. SCOPE

Scrubber Blowdown Rate

III. RESPONSIBIILITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated for the Scrubber Blowdown Rate.

- 1. Check for plugged filter basket at blowdown pump.
 - a. Clean filter basket if needed.
- 2. Check for restrictions in piping and/or Worchester valve.
 - a. Clean/replace if needed.
- 3. Check for plugged discharge hose.
 - a. Clean/replace if needed.
- 4. If flowmeter needs to be calibrated, call I & E for cleaning and/or calibration.
- 5. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the scrubber blowdown rate.



Policy Number: SSMP 2-09

Effective Date: 9/03 Revised: 10/03

MINIMUM SCRUBBER TANK LIQUID LEVEL

PURPOSE

Provide a procedure to investigate the possible reason(s) for the Scrubber Tank Liquid Level to exceed the span limits or fall below the 40% minimum tank level.

П. SCOPE

Scrubber Tank

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. **PROCEDURES**

To ensure that emissions are minimized, the following systems should be investigated for the Scrubber Tank Liquid Level decrease.

1. Loss of Make-up Water

> This happens due to the loss of Plant or City water flow. If system is running on Plant water when flow stops, change valves so system will run on City Water. If system is running on city water when flow stops, change valves so system is running on Plant water.

When plant water flow stops, check the following:

- Check clean water tank for water level.
- If tank is full, but pump is not running-switch to city water.
 - a. Switch to City water-open primary waterline in city water building and close quarry water lines in Kiln 1 Scrubber.
- If clean water tank is full and pumps are running and city water flow cannot refill tank, then both Kilns/Scrubbers have to be shutdown.

When city water flow stops, check the valves in the City water building, if nothing is wrong, then call Kiln supervisor.

- 2. Restriction at Venturi discharge.
 - Shutdown kiln/scrubber and clear restriction.
- 3. Check for blockage at bottom of Ducon.
 - Close 4" valves at Ducon and return to recycle tank.
 - b. Disconnect 4" hose off Ducon tank.
 - i. Check hose for clockage.
 - ii. Open 4" valve at Ducon and check for flow, clear if necessary.
 - iii. If valves do not close, Kiln will have to be shutdown.
- 4. Check flowmeter, call I&E to clean and/or recalibrate, if needed.
- To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the scrubber tank liquid level.



Policy Number: SSMP 2-10

Effective Date: 9/03 Revised: 10/03

MINIMUM SCRUBBER RECIRCULATION RATE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the Scrubber Recirculation Rate to exceed the span limits or fall below the 175 gallons per minute (gpm) minimum.

II. SCOPE

Scrubber Recirculation Rate

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated for the Scrubber Recirculation Rate. There are two pumps for the scrubber recirculation, if one fails, switch to alternate and check the bad pump for the following to get it back online.

- 1. Check for loss of the pump, switch to alternate pump if needed.
- 2. Check for a loss of the prime.
- 3. Re-prime if necessary.
- 4. Check for plugged headers.
- 5. Replace or clean headers if necessary.
- 6. Check for a plugged basket on recycle pump.
- 7. Clean baskets if necessary.
- 8. If both pumps are online and rate falls below 175 gpm, put Kiln on fossil fuel and insure LGF flow has been automatically shut-off to minimize emissions.

<u>Instrumentation</u>-Insure the instrument that measures scrubber recirculation rate is operating correctly. Call I&E if problematic.



Policy Number: SSMP 2-11

Effective Date: 9/03

Revised: 10/03

MINIMUM SCRUBBER LIQUID pH

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the Scrubber Liquid pH to exceed span limits or fall below the 1.9 pH minimum.

II. SCOPE

Scrubber Liquid pH

III. RESPONSIBIILITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated for the Scrubber Liquid pH.

- 1. Restricted Flow
 - -Check for return flow back into caustic tank in Soda Ash building.
 - a. If flow is strong, restriction is in scrubber building.
 - i. Close and drain feed/return caustic lines.
 - ii. Disconnect piping and clear restriction.
 - b. If flow is weak
 - i. Close feed line at its initial starting point at manifold in Soda Ash building.
 - ii. Clear restriction in feed line.
- 2. Failure of Caustic Feed System
 - a. Loss of prime on pump.
 - i. Re-prime pump.
 - b. Pump failure.
 - i. Switch to back-up pump.
 - ii. Repair old pump.
- 3. Loss of Soda Ash
 - a. Check to make sure feed auger is working.
 - b. Turn on vibrators to losen soda ash that has bridged in silo system.
- 4. Insure instrumentation that measures pH is operating correctly. Call I&E if problematic.
- 5. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result scrubber liquid pH.



Policy Number: SSMP 2-12

Effective Date: 9/03

Revised: 10/03

DRY SORBENT (LIME) FEED RATE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the Dry Sorbent Feed Rate to exceed the span limits or to fall below the 200 pounds an hour (lbs/hr) minimum.

II. SCOPE

Dry Sorbent Feed Rate

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated for the Dry Sorbent Feed Rate.

- 1. LIME FEEDER STOPPAGE
 - a. Switch drive to manual and try to reset.
 - b. Diagnose problem.
 - c. Switch kiln to back-up feeder while repairs can be made.
- 2. LIME ROTARYVALVE STOPPAGE
 - a. Manually try to restart valve.
 - b. Switch kiln to back-up feeder while repairs can be made.
- 3. BLOWERS: 4 TOTAL, 2 BACK-UP
 - a. Check motor/drive belts are operational.
 - b. Manually try to re-start
 - c. Switch kiln to back-up blower.
 - d. Insure instrumentation is operational.
 - e. Disassemble piping to check for restrictions.
- 4. INSTRUMENTATION-Insure instrumentation that measures lime feed rate is operating correctly. Call I&E if problematic.

To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the dry sorbent feed rate.



Policy Number: SSMP 2-13

Effective Date: 9/03

MINIMUM DRY SORBENT (LIME) CARRIER FLUID FLOW RATE

Revised: 10/03

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the Dry Sorbent (Lime) Carrier Fluid Flow Rate to exceed the span limits or fall below the 150 cubic feet per minute (cfm) minimum.

II. SCOPE

Dry Sorbent Carrier Fluid Flow Rate

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated for the Dry Sorbent Carrier Fluid Flow Rate.

- 1. Refer to SOP SSMP 2-12 for procedures on the blowers.
- 2. Insure instrumentation that measures lime flow rate is operating correctly. Call I&E if problematic.
- 3. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the dry sorbent carrier fluid flow rate.



Policy Number: SSMP 2-14

Effective Date: 9/03

Revised: 10/03

KILN PRESSURE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the Kiln Pressure to exceed the span limits or rise above the standard of 0.00 water gauge (wg).

II. SCOPE

Kiln Pressure

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems be investigated for the Kiln Pressure.

- 1. Verify coller discharge doors are clear of excess aggregate.
- 2. Verify operation of ID/Front Barron fan.
- 3. Increase ID/Baron fan, if possible.
- 4. Adjust BHDP down, if possible. (SSMP 3-02).
- 5. Check Venturi/Ducon D.P.
- 6. Verify operations of Heat Exchanger fans/Dilution Damper.
- 7. Unstable Fuel Flow/Unstable Fire.
 - a. Increase ID Fan, if possible.
 - b. Decrease cooler fan(s).
- 8. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result negative kiln pressure no longer being negative.



Policy Number: SSMP 2-15

Effective Date: 9/03

HIGH CARBON MONOXIDE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the condition of High Carbon Monoxide.

II. SCOPE

High Carbon Monoxide

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated should the Carbon Monoxide emissions increase towards the WFCO limit of 100 parts per million (ppm), on a one minute average.

- 1. Loss of Pilot.
 - a. Reset semi-auto Maxon valve.
 - b. Start/depress pilot until flame has ignited.
 - c. Add fossil fuel until CO hourly rolling average (hra) is within the limits.
 - d. Switch to LGF.
- 2. Unstable Fuel.
 - a. Switch to fossil fuel if CO is greater then 75 ppm hra.
 - b. Wait until CO is below 75 ppm hra before switching back to LGF.

The limit for CO varies for each type of fuel.

CO alarm limits: LGF-75 ppm hra

Kiln Oil- 500 ppm hra Natural Gas-none

- 3. Insure instrumentation that measures CO is operating correctly. Call I&E if problematic.
- 4. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result high CO.



Policy Number: SSMP 2-16

Effective Date: 9/03 Revision Date: 8/04

MINIMUM LGF ATOMIZATION AIR PRESSURE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the condition of Minimum Atomization Air Pressure.

II. SCOPE

Minimum Atomization Air Pressure

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated should the Minimum Atomization Air Pressure reach a level of 52 psig.

1. Check to see if main air compressor is running.

If Not Running:

- Restart Compressor;
- If No restart, connect portable air compressor to main feed lines.

If Running:

- Check for leaks in air system;
- Call I&E for calibration of instrument
- 2. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the minimum atomization air pressure.



Policy Number: SSMP 2-17

Effective Date: 9/03

Revised: 10/03

POWER FAILURE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for a Power Failure.

II. SCOPE

Power Failure-Loss of Operations

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

The following procedures should be followed in the event of a loss of power.

- 1. Total Power Loss (Operations)
 - a. Electrically disconnect kiln(s)
 - b. Couple kiln(s) to Pony Drive.
 - c. Start Pony Drive and begin to turn kiln(s).
- 2. Total Power Loss (Kiln Operator-Burner)
 - a. Close LGF vent valve(s).
 - b. Manually close all LGF and waste oil valves.
 - c. Close water supply valve to burner.
 - d. Close Gas/Pilot valves to "Off" position.
- 3. Sporadic Power Loss
 - Identify equipment that has been affected.
 - b. Try to restart equipment.
 - i. If equipment does not restart, processes may need to be shut down, (i.e. fire/shale) as not to cause damage.
- 4. Restart/Re-energize by list of importance (if not already running)
 - a. Recycle pump, quench pump, blowdown pump and clean water pump at WWTP.
 - b. ID fan.
 - c. Kiln drive.
 - d. Heat exchanger fans.
 - e. Re-light fire.
 - f. Soda ash pump/mixers.
 - g. Cooler fans, drive, screws, front barron fan.
 - h. Clinker conveyor.
 - i. Lime system.
 - j. APC equipment.
 - k. Shale conveyors.
 - 1. LGF/Waste oil pump on at Fuel Farm.
 - m. Shale on after kiln has been re-heated.
- n. LGF on, after all parameters are in compliance.

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Policy Number: SSMP 2-18

Effective Date: 9/03 Revised: 10/03

LOSS OF ID FAN

I. PURPOSE

Provide a procedure to restart the Induced Draft (ID) Fan in case of loss or span limit exceedance.

II. SCOPE

ID Fan

III. RESPONSIBILITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated should the ID Fan exceed span limits or exceed 405 amperes.

- 1. Re-start Fan.
- 2. If fan will not restart, open dilution damper to 100%, then call I & E to diagnose the problem.
- 3. To assure that emissions are minimized during this procedure, insure that LGF flow has been automatically discontinued as a result of the ID fan exceeding 405 amperes.
- 4. Insure the instrument that measures ID fan amps is operating correctly. Call I&E if problematic.



Policy Number: SSMP 2-19

Effective Date: 9/03

DILUTION DAMPER

I. PURPOSE

Provide a procedure to investigate the loss of the Dilution Damper.

II. SCOPE

Dilution Damper

III. RESPONSIBILITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

- 1. Adjust Heat Exchanger fans.
- 2. If not possible-manually adjust damper by disconnecting control arm.
- 3. Lower ID fan.
- 4. If none of the above remedy situation, Flame out/Shut down until repairs are completed.
- 5. Insure instrumentation that measures dilution damper is operating correctly. Call I&E if problematic.

To assure that emissions are minimized during this procedure, insure that LGF flow has been automatically discontinued as a result of the dilution damper.



Policy Number: SSMP 2-20

Effective Date: 9/03 Revised: 10/03

LOSS OF LGF FLOW

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the LGF Flow to exceed span limits or be lost.

II. SCOPE

LGF Flow

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following steps should be taken for the flow of LGF.

LGF Line

- 1. Manually open/close LGF valves.
- 2. Close OPCO/WFCO valve then used piped in water to flush lines.
- 3. Take apart and check for obstruction

Loss of flow from Pump/Low Pressure

- 1. Check tank screen to see if pump is running. Restart/Reprime pump.
- 2. Close down on recirculation valve in EQ room to increase pressure.

Instrumentation

1. Insure the instrument that measures LGF flow is working correctly. Contact I&E is problematic.



Policy Number: SSMP 2-21

Effective Date: 9/03

Revised: 10/03

LOSS OF SHALE FEED

PURPOSE I.

Provide a procedure to investigate the possible reason(s) for the Loss of Shale Feed or span limit exceedance.

III. SCOPE

Shale Feed

Ш. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. **PROCEDURES**

To ensure that emissions are minimized, the following steps should be taken for the Shale Feed.

The possible reasons for the loss of shale feed are: stoppage of belts, stoppage/loss of rotary valve or stoppage of feed from silo.

- 1. Stoppage of Belts.
 - a. Identify problem, make repairs and then go back on line.
 - To minimized emissions, if repairs are not made within 25 minutes, kiln operator b. must go OFF of LGF until shale can be reintroduced into kiln.
- 2. Stoppage or Loss of Rotary Valve
 - Check for blockage of chute into kiln. a.
 - b. If chute is plugged, manually clean out.
 - Check to make sure rotary valve is functional. c.
 - d. To minimized emissions, if repairs are not made within 25 minutes, kiln operator must go OFF of LGF until shale can be reintroduced into kiln.
- 3. Stoppage of Feed from Silo

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- Check for large stones or frozen material blocking chute from silo. a.
- **b**. If blocked, chute must be cleaned and freed of blockage.
- To minimized emissions, if repairs are not made within 25 minutes, kiln operator c. must go OFF of LGF until shale can be reintroduced into kiln.

Instrumentation-Insure instrument that monitors shale feed is working correctly. Call I&E if problematic.

Norlite, LLC



Policy Number: SSMP 2-22

Effective Date: 8/04

MINIMUM LIQUID TO GAS RATIO (L/G)

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for the minimum liquid to gas ratio to fall below the minimum limit of 4.0 gallons/1000 wet scfm.

II. SCOPE

Minimum Liquid to Gas Ratio

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following steps should be taken for the liquid to gas ratio.

- 1) Check for low recycle flow;
- 2) Check for low gas flow rate and/or check ID fan settings.
- 3) Call I&E.

To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the liquid to gas ratio.



NORLITE CORPORATON
Policy Number: SSMP 2-23

Effective Date: 8/04

MAXIMUM HEAT EXCHANGER EXIT TEMPERATURE

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for exceeding the span limits or the maximum Baghouse Inlet Temperature of 400°F.

II. SCOPE

Heat Exchanger Exit Temperature

III. RESPONSIBILITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

To ensure that emissions are minimized, the following systems should be investigated should the Maximum Heat Exchanger Exit Temperature (hra) exceed 453°F.

- 1) If possible, increase fan speed of Heat Exchanger fans as needed.
- 2) Check to see if both Heat Exchanger fans are operational.
- 3) Insure instrumentation of Heat Exchanger Exit Temperature is operational, Call I&E.

To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of the maximum heat exchanger exit temperature.



Policy Number: SSMP 3-01

Effective Date: 9/03

HEAT EXCHANGERS

I. PURPOSE

Provide a procedure to investigate the possible reason(s) for a malfunction of the Heat Exchangers.

II. SCOPE

Heat Exchangers

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

In order to minimize emissions, the following systems should be investigated should there be a malfunction of the Heat Exchangers.

- 1. Check Heat Exchanger drive for root cause (belts, motors, etc....).
- 2. If OK, restart fan.
- 3. If unable to restart fan, use dilution damper to lower inlet temperature.
- 4. It is possible to run kiln on one fan.
- 5. Evaluate air flow thru tubes in Heat Exchanger. If a large number of tubes have restricted flow, the heat exchanger needs to be cleaned.
- 6. Total loss of both fans.
 - a. Lower ID fan.
 - b. Increase Barron fan.
 - c. Kiln flameout/shutdown until repairs are made.
- 7. Call I & E to diagnose problem and to check instrumentation.
- 8. To assure that emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of loss of heat exchangers.



Policy Number: SSMP 3-02

Effective Date: 9/03

BAGHOUSE MALFUNCTION

PURPOSE T.

Provide a procedure to investigate the possible reason(s) for a malfunction of the Baghouses.

II. SCOPE

Baghouses

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. **PROCEDURES**

In order to minimize emissions, the following systems should be investigated should there be malfunction of the Baghouses.

- 1. Bag Leak Detection Alarm activated in burner control room. NOTE: Must initiate procedures used to determine cause of alarm w/in 30 minutes of the time alarm first sounds.
 - a. Notify Trunnion operator of alarm.
 - b. Initiate completion of SSMP 3-04A-Operators Checklist

The following may be necessary to alleviate the cause of the alarm.

- Inspect baghouse for air leaks, torn or broken filter elements or other malfunctions
- b. Seal off defective baghouse
- c. Clean the bag leak detection probe, or otherwise repairing the bag leak detection system. (Contact I&E)
- d. Shut down kiln.
- e. Refer to SOP **OM 2-03** for procedure for bag replacement.

2. High or Low Baghouse Differential Pressure (BHDP)

(referenced with low venturi pressure)

- a. High BHDP
 - i. Adjust needles on magnahelic indicators (in MCC) to lower DP-both red needles turned counter clockwise past black needle

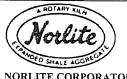
OR

- ii. Check for leaks at ASCO valves on top of baghouse.
- iii. Check air to pulsers (65-70 psi minimum).
- iv. Check/clean overall DP sample lines in baghouse duct work.

b. Low BHDP

i. Adjust needles on magnahelic in MCC room. Turn dials clockwise so both red needles go past black needle. This will stop pulsing of baghouse to increase DP.

Cohoes, New York



Policy Number: SSMP 3-03

Effective Date: 9/03 Revised: 10/03

DUCON AND VENTURI SCRUBBERS

I. **PURPOSE**

Provide a procedure to investigate the possible reason(s) for a malfunction of the Ducon and Venturi Scrubbers.

II. **SCOPE**

Ducon and Venturi Scrubbers

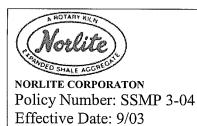
III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. **PROCEDURES**

To minimize emissions, the following systems should be investigated should there be malfunction of the Ducon and Venturi Scrubbers.

- 1. Ducon Scrubber Malfunction
 - a. High DP Across Ducon Scrubber
 - i. Loss/Reduction of flue gases thru scrubber
 - 1. Shutdown Kiln to inspect/clean.
- 2. High DP across Venturi
 - a. Loss/Reduction of flue gases thru Venturi.
 - i. Increase Quench water flow to clear.
- 3. Failure of Scrubbers
 - a. Shutdown Kiln to insect/clean.
- 4. Insure instrumentation that measures scrubbers is operating correctly. Call I&E if problematic.
- 5. To assure emissions are minimized during this procedure, insure that LFG flow has been automatically discontinued as a result of scrubber pressure drop.



MACT FIELD OPERATORS CHECKLIST

I. PURPOSE

Provide a checklist to ensure Kiln(s), Air Pollution Control Equipment and Monitoring Equipment are operated within parameters of MACT Plans.

II. SCOPE

Kiln(s), Air Pollution Control Equipment and Monitoring Equipment

III. RESPONSIBILLITIES

Kiln Burner Operators, Kiln Supervisors or Instrumentation and Electrical Department (I & E)

IV. PROCEDURES

Refer to SSMP 3-04A for checklist form.

1. Kiln Operators, Supervisors or the I & E department are to fill out the checklist each time there is a startup, shutdown or malfunction of the kilns, air pollution control equipment or monitoring equipment.

MACT Startup, Shutdown and Malfunction Plan Kiln Burner Operator's Checklist During S, S and M.

This form is to be filled out during a Startup, Shutdown or Malfunction of the Kiln, Air Pollution Control (APC), Monitoring Equipment or a Bag Leak Alarm.

Date:	: P	erson Com	pleting Form: _	F1140-		Shift:						
Circle E (Requ		Startup	Shutdown		Malfunction		Bag Leak Alarm NOTE: (Must start procedures to decide cause of alarm w/in 30 minutes					
Circle E (Requ		APC	Monitoring Eq	uipment	Kiln 1	Kiln 2	of time alarm first sounds.)					
Explain Oc	currence:			7650								
Startı	up/Shutdown Tin	nes			В	_	Detection Alarm Alarm Activated:					
Time System We (Off All F Time System Car	uels)		- - - ,		Time		leasures began:					
	art of Procedures), Time is fro	om DEC Report)]				174 4					
T	alfunction Times		1 .			Office 11-1						
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I IIIIe Ev	ent Corrected:		Operator should i	•								
			which SOP's were Operator's	e tollowed.			unctions					
OP #	Descript	tion	Initials				sures that were done to					
Operations:	Startu		muais		correct malf	unction:						
SSMP 2-01	Kiln Startup											
201	ram otartap	Oolu										
SSMP 2-02	Kiln Startup	-Warm										
001111 2 02	Shutdov											
SSMP 2-03	Kiln Shutdown											
2 00	Tan Onataown	i idililod	A									
SSMP 2-03A	Kiln Shutdown-E	Emergency										
	or Unexpe		What is a second with the second second									
SSMP 2-17	Power Fa											

Continuous M	onitoring Systems	s (CMS):			İ							
SSMP 4-01	Startu											
SSMP 4-02	Power Fa	ilure										
SSMP 4-03	Malfunct	ion				**						
SSMP 4-04	Shutdov	wn										
	actions taken not	in SOP's:										
Kev:												

Malfunction: any sudden, infrequent, and not reasonably preventable failure of air pollution control equipment, process equipment, or a rocess to operate in a normal or usual manner. Failures that are caused in part by poor maintenance or careless operation are not malfunctions.

Shutdown: the stoppage of operation of an affected source or portion of an affected source for any purpose.

Startup: the setting in operation of an affected source or portion of an affected source for any purpose.



Policy Number: SSMP 4-01

Effective Date: 9/03

CONTINUOUS EMISSIONS MONITORING

SYSTEM-STARTUP

I. PURPOSE

Provide a procedure for the startup of the Continuous Emissions Monitoring System (CEMS).

II. SCOPE

Continuous Emissions Monitoring Systems

III. RESPONSIBIILITIES

Instrumentation and Electrical Personnel (I & E)

IV. PROCEDURES

Refer to the CISCO Operations and Maintenance Manual, dated December 1995, Section 3: SYSTEM START-UP/CHECKOUT.



Policy Number: SSMP 4-02

Effective Date: 9/03

CONTINUOUS EMISSIONS MONITORING

SYSTEM - POWER FAILURE

I. PURPOSE

Provide a procedure for a power failure of the Continuous Emissions Monitoring System (CEMS).

II. SCOPE

Continuous Emissions Monitoring Systems

III. RESPONSIBILLITIES

Instrumentation and Electrical Personnel (I & E)

IV. PROCEDURES

The CEMS is connected to an Uninterrupted Power Source (UPS) battery backup which is capable of operating the CEMS system for approximately 30 minutes after a power failure.

All CEMS data will be backed up while the UPS is operating. Any extended power failure (exceeding 30 minutes) affecting the CEMS would also affect the kilns and associated air pollution control equipment, therefore, no emission would be generated due to the kilns being shutdown for longer than 30 minutes.

To restart CEMS, refer CISCO Operations and Maintenance Manual, Dated 1995, Section 3



Policy Number: SSMP 4-03

Effective Date: 9/03

CONTINUOUS EMISSIONS MONITORING SYSTEM-MALFUNCTION

I. PURPOSE

Provide a procedure to follow during a malfunction of the Continuous Emissions Monitoring System (CEMS).

II. SCOPE

Continuous Emissions Monitoring Systems

III. RESPONSIBILLITIES

Instrumentation and Electrical Personnel (I & E)

IV. PROCEDURES

"Faulty CEM" light starts to flash in control room.

- 1. Switch to gas or oil (if approved to burn as virgin fuel).
- 2. Notify Supervisor
- 3. Contact I&E.
- 4. Wait for supervisor's approval to begin burning waste fuel.



Policy Number: SSMP 4-04

Effective Date: 9/03

CONTINUOUS EMISSIONS MONITORING SYSTEM

I. PURPOSE

Provide a procedure to follow during the shutdown of the Continuous Emissions Monitoring System (CEMS).

II. SCOPE

Continuous Emissions Monitoring Systems

III. RESPONSIBIILITIES

Instrumentation and Electrical Personnel (I & E)

IV. PROCEDURES

The CEMS is on-line continuously, for 24 hours a day, 7 days a week and 365 days a year.

The only exception is when an upgrade to the PCL and DAS is required. The kiln and all associated air pollution control equipment would also be shut down before the CEMS was placed off-line.



Policy Number: OM 2-02

Effective Date: 9/03

TANK SWITCH-AFTER HOURS

I. PURPOSE

Provide a method for proper lockout of LGF storage tanks in the Fuel Farm during the hours when Fuel Farm employees are *not blending or unloading LGF*, so as to avoid the inadvertent introduction of incompletely blended LGF into the kiln burner system.

II. SCOPE

Fuel Farm

III. RESPONSIBIILITIES

Kiln Supervisor

IV. PROCEDURES

With the exception of the current burn tank, all tanks capable of being put on the LGF raceway (burn tanks) will be locked out during non-blending or unloading hours, typically nights and weekends.

A. Responsibilities

- 1. Fuel Farm personnel will be required to lock out all LGF burn tanks on a daily basis at the end of blending and unloading operations, with the exception of the in process burn tank. The employee performing lockout activities will sign off that lockouts were completed on the daily Unloading/Transfer sheet.
- 2. Lab personnel will be responsible for performing a visual check verifying that all LGF tanks are properly locked out, with the exception of the burn tank. The visual check will be performed any day that a Shift Supervisor Burn Log sheet is issued. The tank status will be noted on the burn instructions to the kiln operators/shift supervisors.
- 3. The kiln supervisor is responsible for switching burn tanks according to the procedures set forth in Section B below.

B. Tank Switching/Lockout Procedures

Each burn tank will have its own dedicated lockout box with three (3) keyed-alike dedicated locks.

- 1. Before a burn tank switch is performed, the kiln operator(s) will switch to non-LGF fuel (i.e. oil).
- 2. The pump for the empty burn tank will be shut down and the bottom suction line valve, the top suction line valve, and the raceway return line valve will be closed and locked out with the dedicated locks from the appropriate lockout box.
- 3. The next burn tank's valves, top or bottom suction valve and the raceway return valve, will be unlocked and opened to the kiln. The locks will be returned to the appropriate dedicated lockout box.
- 4. The pump for the new burn tank will be started and flow to the kiln(s) will be established.
- 5. Within fifteen (15) minutes after LGF flow has been established to the kiln(s) after a tank switch, the kiln supervisor will verify that the tank switch was performed correctly. This will be accomplished by checking level gauges, the safety vent overflow line, and the alarm log on the LGF panel screen for rupture disc failures. During this 15-minute interval, the kiln supervisor will perform a walk through of the entire fenced in area of the Fuel Farm. This will be documented as part of the security rounds on the Security Check sheet.
- 6. An incident report will be completed by a responsible party as outlined in Section A any time there are less than 3 burn tanks locked as described in these procedures.



Policy Number: OM 2-03 Effective Date: 9/03

BAGHOUSE-BAG CHANGING

I. PURPOSE

Provide a procedure for the correct change-out of the bags in the baghouses.

II. SCOPE

Baghouses

III. RESPONSIBIILITIES

Kiln Maintenance Worker

IV. PROCEDURES

After it has been identified there is a bad bag in the baghouse, follow the following steps for changing the bag(s) out:

- 1. Kiln goes to gas for a minimum of 30 minutes.
- 2. Close Inlet and Outlet Dampers.
- 3. Open Baghouse Door, follow proper entry procedures.
- 4. Enter Baghouse.
- 5. Identify a bad bag and/or also check the bag leak detection system.
- 6. If bad bag proceed to Step 7, if no bad bags, call I & E to investigate bag leak detection system.
- 7. Pull blow tube.
- 8. Pull cage and bag.
- 9. Separate the bag from the cage.
- 10. Replace bag.
- 11. Notify Kiln Control of bag replacement.



Policy Number: OM 2-04 Effective Date: 9/03

LWAK, MULTICLONE, AIR TO AIR HEAT EXCHANGER, VENTURI SCRUBBER, MIST ELIMINATOR, ID AND FD FANS

I. PURPOSE

Provide a procedure that ensures the inspections and monitoring of the operating systems located in "SCOPE".

II. SCOPE

Lightweight Aggregate Kilns (LWAK), Air to Air Heat Exchanger, Venturi Scrubber, Mist Eliminator, ID and FD Fans.

III. RESPONSIBILLITIES

Kiln Burner Operators and Kiln Supervisors

IV. PROCEDURES

The operating procedures for the systems listed in the "SCOPE" consist of multiple daily physical inspections, instead of a detailed step-by-step operational procedure. Each system is continually monitored to ensure it is within in the operational ranges. Below is a description of the inspections that occur at each area.

LWAK

The LWAK is made up of multiple systems. The Kiln Burner Operator is responsible for continually monitoring the LWAK system and the Kiln Shift Supervisor and Trunnion Operator will conduct a daily physical inspection of the system. The inspection sheets that are used to monitor the LWAK system are Attachments OM 2-04A and OM 2-04B.

MULTICLONE

The Wastewater Treatment Shift Operator is responsible for inspecting the Multiclone. The operator uses the inspection sheet, OM 2-04C, to record the results of the inspection.

AIR TO AIR HEAT EXCHANGER

The Trunnion Operator is responsible for inspecting the Air to Air Heat Exchanger. The operator uses the inspection sheet, OM 2-04A, to record the results of the inspection.

VENTURI SCRUBBER

The Trunnion Operator is responsible for inspecting the Venturi Scrubber. The operator uses the inspection sheet, OM 2-04A, to record the results of the inspection.

MIST ELIMINATOR

The Trunnion Operator is responsible for inspecting the Mist Eliminator. The operator uses the inspection sheet, OM 2-04A, to record the results of the inspection.

ID AND FD FANS

The Kiln Burner Operator is responsible for continually monitoring the ID and FD fans system and the Kiln Shift Supervisor and Trunnion Operator conduct random visual inspections of the system.

Insure instrumentation that measures the above mentioned machinery is operating correctly. Call I&E if problematic.

OM 2-04A KILN FIELD OPERATORS SHIFT REPORT

1E			DATE			SHIF	Τ	
ERVISORS SI	GNATURE:_			·	····			
ATER READIN	IGS AND SIL	O LEVELS						
QUARRY/CITY KILN1 QUARR	WATER REA		STAR	RT		END		GALLO
KILN 1 CAUST	IC TOTALIZER			****				
	RY/CITY WATER	TOTALIZER						-
	IC TOTALIZER						-	
SODA ASH MA	KE-UP TOTALIZI	≣R						
LIME SILO LEV	/EL		TIME					
SODA ASH SIL	O LELEL		TIME					
					<u> </u>	*************************************		
KILN 1	OIL LEVEL OK	AMOUNT ADDED	SEAL OK	KILN 2		OIL LEVEL OK	AMOUNT ADDED	SEAL OK
PIER 1 NE		ADDLD		PIER 1	NE		ADDED	
PIER 1 SE				PIER 1	SE			
PIER 1 NW				PIER 1	NW			
PIER 1 SW				PIER 1	SW			
PIER 2 NE				PIER 2	NE			
PIER 2 SE				PIER 2	SE			
PIER 2 NW				PIER 2	NW			
PIER 2 SW				PIER 2	SW			
*NOTE DIED	1.70.070001400			PIER 3	NE			
"NOTE PIEK	1 IS DISCHARG	E PIEK"		PIER 3	SE			
				PIER 3	NW			
				PIER 3	SW			
DO OIL DRUM	S NEED TO BE EM	PTIED AT KILN 27	?			PIER 1	PIER 2	PIER 3
KILN 1 PIERS								
KILN 2 PIERS						1	1	1

BULL GEAR, PINNION GEAR AND DUST SEAL INSPECTIONS

	KILN 1	KILN 2	
KILN 1 BULL GEAR GREASED AND KILN 2 OIL LEVEL KILN 2 OIL LEVEL CHECKED			WAS OIL ADDED TO KILN2 GEAR
PINION BEARINGS (EAST AND WEST) GREASED			
# OF FEED SEALS MISSING			
# OF DISCHARGE SEALS MISSING			
KILN 1 ANY MAINTENANCE REQUIRED IN THIS	AREA	, 11, 2 <u>0</u>	
KILN 2 ANY MAINTENANCE REQUIRED IN THIS	AREA	,	

LIME FEEDERS, ROTARY VALVES AND BLOWER INSPECTION- RECORD ALL CHANGES *USE ADDITIONAL SHEETS AS REQUIRED

FEEDING KILN	TIME	SETTING *NOT FROM WAP 2- ACTUAL SETTING*	LIME	FEE	DER	ROTA	RY VALVE	BLO'	WER	SELE	CTED
KILN 1		lbs./hr	1	2	3	ON	OFF	А	В	С	D
KILN 2		lbs./hr	1	2	3	ON	OFF	Α	В	С	D
KILN 1		lbs./hr	1	2	3	ON	OFF	Α	В	С	D
KILN 2		lbs./hr	1	2	3	ON	OFF	Α	В	С	D
KILN 1		lbs./hr	1	2	3	ON	OFF	Α	В	С	D
KILN 2		lbs./hr	1	2	3	ON	OFF	Α	В	С	D
KILN 1		lbs./hr	1	2	3	ON	OFF	Α	В	С	D
KILN 2		lbs./hr	1	2	3	ON	OFF	Α	В	С	D

ARE ALL LIME FEEDERS GUARDED- REPORT CONDITION	

IS LIME SILO CLEAN AND FREE OF SPENT LIME- REPORT CONDITION

		OIII = 0 17 (
	IS ANY MAINTENANCE REQUIRED IN THIS AREA			
		*.** *:: <u>***************************</u> *, **		
	\			N.
ace ^{nt}	NAME:	DATE:	SHIFT:	

SCRUBBER SYSTEM INSPECTION

					KILN 1				KILN 2		
RECYCLE PUMP RUNNING				NO	RTH OR	SC	UTH	NORTH	OR	SOUT	Н
RECYCLE PUMP LEAKING			,	YES	OR OR	NO		YES	OR	NC)
BLOWDOWN PUMP LEAKING				YES	G OR	NO		YES	OR	NO	
KILN 1 QUENCH WATER SETTIN	GS	1		2			3	De Brenning Sterensberg Start Start H	4		
KILN 1 MIST PAD WATER SETTI	NG	Вликовором			*NOTE-READ TOTAL QUEN					LOAT	are the process of the seasons of
KILN 2 QUENCH WATER SETTIN	GS	1		2			3	Antale Color of Tues Parcing Con-	4	politica de la companya de la compa	
KILN 2 MIST PAD WATER SETTI	NGS	(Padanguranne):				oligi (lating futorium)			spilinger in anggenomen	<u>ของ (เพราะสัตรายเมลุ่กคาก</u> ร	
KILN 1 QUENCH PUMP RUNNING	YES	OR	NO		N 1 EMERGE LVES OPEN	NCY (UENCH		YES	OR	NO
KILN 2 QUENCH PUMP RUNNING	YES	OR	NO	H	N 2 EMERGE LVES OPEN	NCY (UENCH		YES	OR	NO
KILN 1 SCRUBBER- IS ANY MAIN	TENANO	CE REQ	UIRED IN T	HIS AREA	\?						
ILN 2 SCRUBBER- IS ANY MAIN	TENAN	CE REQ	UIRED IN T	HIS AREA	۱?						

SODA ASH BUILDING

			KILN 1	KILN 2	TIME	CONCENTRATION
NORTH PUMP FEEDING KILN				1		
IS PUMP LEAKING	YES	NO				
SOUTH PUMP FEEDING KILN						
IS PUMP LEAKING	YES	NO				
SODA ASH SCREW-REPORT CONDITION						
ARE ALL COVERS IN PLACE	YES	NO				
ARE ALL GUARDS IN PLACE	YES	NO				
SODA ASH MIXERS RUNNING- REPORT CONDITION					·	
IS ANY MAINTENANCE REQUIRED IN THIS AREA						

HEAT EXCHANGER FANS, PRIMARY AIR FANS, KILN 2 DRIVE AND SILO HEAT INSPECTION

Appendix CAA E

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YES NO	KILN 1 LOWER HEAT EXCHANGER FAN GREASED	YES NO
YES NO	KILN 1 LOWER (OLD) FAN RUNNING	YES NO
HZ	KILN 2 MAIN DRIVE	HZ
	YES NO	YES NO KILN 1 LOWER (OLD) FAN RUNNING

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KILN 2 HEAT EXCHANGER SETPOINT	HZ	K1 SHALE SILO HEAT RUNNING	YES NO	
KILN 1 PRIMARY AIR FAN SETPOINT	HZ	IS ANY-MAINTENANCE REQUI AREAS?	RED IN-THESE	
KILN 2 PRIMARY AIR FAN SETPOINT	HZ			

NAME:	DATF.	SHIFT:
I ALZIALITE.		OIMII.

RAW SHALE BELTS INSPECTION

	KILN 1 TOP	KILN 1 BOTTOM	KILN 2 TOP	KILN 2 MIDDL	E	KILN	N 2 BOTTOM
SHALE BELTS AND SPLICES IN WORKING CONDITION	YES NO	YES NO	YES NO	YES NO		YES	NO
ROLLERS AND RETURNS IN WORKING CONTITION	YES NO	YES NO	YES NO	YES NO		YES	NO
WIPERS IN PLACE AND IN GOOD CONDITION	YES NO	YES NO	YES NO	YES NO		YES	NO
HEAD PULLEYS AND TAIL PULLEYS GREASED	YES NO	YES NO	YES NO	YES NO		YES	NO
KILN 1 ALL CONVEYOR COVERS AND GUARDS IN PLACE	YES NO	YES NO	YES NO	YES NO		YES	NO
KILN 2 ALL CONVEYOR COVERS AND GUARDS IN PLACE			YES NO	YES NO		YES	NO
ROTARY VALVE- SHALE FEED FOR KILN 1 REPORT CONDITION			ARE GUARDS IN	PLACE	YES	NO	
ROTARY VALVE- SHALE FEED FOR KILN 2 PEPORT CONDITION			ARE GUARDS IN	PLACE	YES	NO	
URATE FEEDER FOR KILN 1 ORT CONDITION			ARE GUARDS IN	PLACE	YES	NO	
ACCDURATE FEEDER FOR KILN 2 REPORT CONDITION			ARE GUARDS IN	PLACE	YES	NO	
KILN 1 SHALE FEED- IS ANY MAINTENANCE REQUIRED IN	N THIS AREA			<u> </u>			
KILN 2 SHALE FEED- IS ANY MAINTENANCE REQUIRED IN	N THIS AREA						

COOLER SYSYTEM AND COOLER FAN INSPECTION

COOLERS AND COOLER FANS KILN 1 KILN 2

COOLER DRIVE SYSTEM GREASED	YES NO	YES NO
BARRON EXHAUST SYSTEM GREASED	YES NO	YES NO
EAST COOLER FAN GREASED	YES NO	YES NO
WEST COOLER FAN GREASED	YES NO	YES NO
KILN COOLER AREAS CLEANED	YES NO	YES NO
COOLER SCREWS RUNNING NORTH	YES NO	YES NO



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	ON Z-0-7/1			
COOLER SCREW RUNNING SOUTH		YES NO	YES 1	10
DUST DRUMS EMPTIED		YES NO	YES N	10
KILN 1 COOLER- IS ANY MAINTENANCE REQUIRED	IN THIS AREA			
KILN 2 COOLER- IS ANY MAINTENANCE REQUIRED	IN THIS AREA			· · · · · · · · · · · · · · · · · · ·
NAME:	DATE:	SHIFT		

CLINKER BELTS AND TUNNEL INSPECTION

		KILN 1	KILN 2
BELTS AND SPLICES IN GOOD CONDITION	YES NO	YES NO	
HEAD PULLEYS AND TAIL PULLEYS GREASED AND GUARDED	YES NO	YES NO	
ROLLERS AND RETURN IN GOOD CONDITION AND GUARDED	YES NO	YES NO	
WIPERS IN PLACE AND IN GOOD CONDITION	YES NO	YES NO	
PUMP IN TUNNEL IN GOOD CONDITION	YES NO	YES NO	
WAS PUMP CHANGED OUT ON YOUR SHIFT	YES NO	YES NO	
CLINKER BELT WATER SPRAYS	ON OFF	ON OFF	
CLINKER BELT HEAD BOX WATER SPRAYS	ON OFF	ON OFF	
TUNNEL CLEAN AT START OF SHIFT	YES NO	YES NO	
TUNNEL CLEAN AT END OF SHIFT	YES NO	YES NO	
ALL CONVEYOR COVERS IN PLACE	YES NO	YES NO	
KILN 1 – ANY MAINTENANCE REQUIRED IN THIS AREA			
KILN 2- ANY MAINTENANCE REQUIRED IN THIS AREA			

AIR COMPRESSORS AND PORTABLE AIR COMPRESSORS

	KILN 1	KILN 2
OIL LEVEL CHECKED	YES NO	YES NO
HOW MUCH OIL WAS ADDED		
AIR COMPRESSOR TEMP		
AIR DRYERS AND AFTERCOOLERS WORKING	YES NO	YES NO

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ON 2-04A		
DRYER RELIEF VALVE WORKING PROPERLY	YES NO	YES NO
PORTABLE COMPRESSOR RUNNING	YES NO	YES NO
FLUIDS CHECKED IN PORTABLE	YES NO	YES NO
PORTABLE RE-FUELED FOR NEXT SHIFT	YES NO	YES NO
ANY MAINTENANCE REQUIRED IN THIS AREA		

NAME:	DATE:	SHIFT:
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SUPERVISOR DAILY KILN INSPECTION

INSPECTIONS TO BE	DONE T	WICE A	SHIFT	KILN # 1
DATE TIME		оит	SIDE TEMP	Supv. Init.
Thrust Button Contact	Uphill	Sec.	Down Hill	Sec.
Thrust Button Housing Temp	Uphill		Down Hill	
Feed Pier Temperature	SE	NE	SW	NW
Discharge Pier Temperature	SE	NE	sw	NW
Shell Condition				
Comments				

			CIUCT	
INSPECTIONS TO BE	DONE T	WICE A		KILN # 1
	DONE T	WICE A		
INSPECTIONS TO BE	DONE T	WICE A	SIDE TEMP	Supv. Init.
INSPECTIONS TO BE	DONE T Uphill	WICE A S OUT Sec.	SIDE TEMP	Supv. Init.
INSPECTIONS TO BE DATE TIME Thrust Button Contact	DONE T Uphill	WICE A S OUT Sec.	SIDE TEMP	Supv. Init.
INSPECTIONS TO BE DATE TIME Thrust Button Contact Thrust Button Housing Temp	Uphill	<i>WICE A</i> . ОUТ Sec.	SIDE TEMP Down Hill Down Hill	Supv. Init Sec.
INSPECTIONS TO BE DATE TIME Thrust Button Contact Thrust Button Housing Temp Feed Pier Temperature Discharge Pier Temperature Shell Condition	Uphill	WICE A SOLUTION OUT Sec.	Down Hill Down Hill SW SW	Supv. Init Sec NW
INSPECTIONS TO BE DATE TIME Thrust Button Contact Thrust Button Housing Temp Feed Pier Temperature Discharge Pier Temperature Shell Condition	Uphill Uphill SE SE	WICE A SOLUTION OUT Sec.	Down Hill Down Hill SW SW	Supv. Init Sec NW

SUPERVISOR DAILY KILN INSPECTION

	- DOIYL I	WICE A		KILN # 2
DATETIME		OUT	SIDE TEMP	Supv. Init.
Thrust Button Contact	Uphill	Sec.	Down Hill	Sec.
Thrust Button Housing Temp	Uphill		Down Hill	
Feed Pier Temperature	SE	NE	sw	NW
Center Pier Temperature	SE	NE	SW	NW
Discharge Pier Temperature	SE	NE	SW	NW
Shell Condition			**************************************	
Other Observations				
	- 10 To 10 MAN - 1			
INSPECTIONS TO BE	DONE T	WICE A	SHIFT	
INSPECTIONS TO BE	E DONE T	<i>WICE A</i> .	S <i>HIFT</i> SIDE TEMP	<i>KILN # 2</i> Supv. Init
INSPECTIONS TO BE DATE TIME Thrust Button Contact	E DONE T	<i>WICE A</i> .	S <i>HIFT</i> SIDE TEMP	<i>KILN # 2</i> Supv. Init
INSPECTIONS TO BE	DONE T	<i>WICE A</i> .	SHIFT SIDE TEMP Down Hill	<i>KILN # 2</i> Supv. Init
INSPECTIONS TO BE DATE TIME Thrust Button Contact Thrust Button Housing Temp	Uphill_	<i>WICE A</i> OUT Sec.	SHIFT SIDE TEMP Down Hill Down Hill	KILN # 2Supv. Init Sec.
INSPECTIONS TO BE DATE TIME Thrust Button Contact Thrust Button Housing Temp Feed Pier Temperature	Uphill	WICE A OUT Sec NE	SHIFT SIDE TEMP Down Hill Down Hill SW	KILN # 2Supv. Init SecNW

KILN DUST LEVEL INSPECTION LOG

_LN 1 BAGHOUSE	TIME 1	MOD A	MOD B	MOD C	ТІМЕ 2	MOD A	MOD B	MOD C	KILN 1 MULTICLONE	HOPPER LEVEL	HOPPER LEVEL
DIFFERENTIAL PRESSURE (IN MCC)			1						TIME 1	UPPER	LOWER
OUTLET FEMPERATURE (IN MCC)									TIME 2	UPPER	LOWER
SUCTION LEVEL OW,MIDDLE, HIGH, NONE									ROTARY VALVE ON	YES OF	R NO
ROTARY VALVE RUNNING									RV MAINT NEEDED	YES OF	R NO
OTARY VALVE DJUSTMENT MADE									BLOWER SELECTED		
AC TRUCK LOADS AKEN									SELECTED	EAST OF	R WEST
OTARY VALVE AINTENANCE NEEDED											
AGHOUSE BLOWER	NORT	H OR	COLITU		MODIL	J 00	POLITIU				**
AGHOUSE DUST LINES TO	SILO-MA	INTNENA	NCE NEED	ED-	NORT	H OR	SOUTH				
MULTICLONE DUST LINES	TO SII O-M	IAINTENIAI	VCE NEED	OFD-						***	
IDENICIONE DOG! LINES		AINIENA	NCE NEEL								
ILN 2 BAGHOUSE	TIME 1	MOD A	MOD B	MOD C	TIME 2	MOD A	MOD B	MOD C	KILN 2 MULTICLONE	HOPPER LEVEL	HOPPER LEVEL
FFERENTIAL RESSURE (IN MCC)									TIME 1	UPPER	LOWER
TLET MERATURE (IN MCC)									TIME 2	UPPER	LOWER
JCTION LEVEL DW, HIGH, NONE									ROTARY VALVE ON	YES OR	NO NO
OTARY VALVE UNNING									RV MAINT NEEDED	YES OF	R NO
OTARY VALVE DJUSTMENT MADE									BLOWER SELECTED	EAST OR	WEST
AC TRUCK LOADS AKEN											
OTARY VALVE AINTENANCE NEEDED											
AGHOUSE BLOWER ELECTED	NORTH	OR S	OUTH		NORTH	OR S	OUTH				
AGHOUSE DUST LINES TO	SILO- MA	INTENAN	CE NEEDE	D-							
MULTICLONE DUST LINES	TO SILO-N	IAINTENA	VCE NEED	DED-							
VAS THE VAC TRUCK CLEA	N AND RE	ADY FOR	YOUR US	E?							
ID YOU EMPTY AND CLEA!	N VAC TRI	JCK AFTE	R YOUR L	JSE?			<u></u>				
			*** •								
AS THE EQ ROOM CLEAN A	AT THE BE	EGINNING	OF YOUR	SHIFT?							
D YOU CLEAN FILTER BAS											
OUID WASTE DRUM LEVEL	. 1/4	1/2 3/4	FULL			PPE \	VASTE DF	RUM LEVE	L 1/4 1/2 3/4	FULL	
EQ ROOM CLEAN AT END	OF SHIFT	? ***			Α	RE DRUM	S AND PAI	LS PROPE	RLY LABELED?		
			AND NO U		8						

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SUPERVISOR

Norlite, LLC Cohoes, New York

NEICVP1120E01

____SHIFT_

DATE_

____ NAME_



Policy Number: OM 3-01

Effective Date: 9/03

PREVENTIVE MAINTENANCE PROGRAM

I. PURPOSE

Provide a consistent and reliable system for the preventive maintenance of plant systems and equipment.

II. SCOPE

Norlite Corporation Facility.

III. RESONSIBILITIES

The maintenance manager has the overall responsibility of the preventive maintenance program.

IV. PROCEDURES

The preventative maintenance system is made up of the following components.

PM Work Orders

A group of preventative maintenance (PM) work orders have been generated for plant systems and equipment. As new equipment is added to the plant, or if experience shows the plant equipment needs additional or different preventative maintenance, new PM work orders are added to the system or existing PM work orders are changed to meet the new requirements.

The PM work orders are divided into the following frequency

Weekly, Monthly, Bi-Monthly, Quarterly, Semi-Annual, and Annual

Each PM work order list the inspection or maintenance activity required.

PM Summary

The PM summary is a file that shows the status of all PM work orders issued.

As a PM work order is generated, the PM summary is updated to show the issue date of that particular PM work order.

When the PM work order is completed, the PM summary is updated to show the completion date

PM Work Order File

After the completed PM work order is entered into the PM summary, the hard copy is filed for future reference.



NORLITE CORPORATON Policy Number: OM 3-02

Effective Date: 9/03

CORRECTIVE MAINTENANCE PROGRAM

I. PURPOSE

Provide a consistent and reliable system for the corrective maintenance of plant systems and equipment.

II. SCOPE

Norlite Corporation Facility.

III. RESONSIBILITIES

The maintenance manager has the overall responsibility of the preventive maintenance program.

IV. PROCEDURES

The corrective maintenance system is made up of the following components.

Routine Inspections

All operating areas perform routine inspections daily. Equipment problems noted on these inspections are addressed immediately or added to the area work list for completion during future overhaul periods

Work list

The work list is divided into the major plant areas such as Kiln 1, Kiln 2, Fuel Farm, Waste Water Treatment, etc.

In addition, each area division is made up of two groups of information.

Outage Routines

The outage routine is the day to day schedule used to coordinate maintenance activities and personnel during plant shutdowns.

The outage routine is generated using the area work list future maintenance and repair entries.

When the outage is over, the outage routine is used to update the work list completed maintenance and repair entries.

Outage Routine File

At the end of an area outage, a hard copy of the complete outage routine is filed for future reference.



NORLITE CORPORATON Policy Number: OM 3-03

Effective Date: 9/03

SPARE PARTS MAINTENANCE PROGRAM

I. PURPOSE

Provide a consistent and reliable system for the control and replacement of spare parts involved in the maintenance of plant systems and equipment.

II. SCOPE

Norlite Corporation Facility.

III. RESONSIBILITIES

The maintenance manager has the overall responsibility of the spare parts maintenance program.

IV. REFERENCES

Spare parts for the plant equipment are controlled as follows.

Equipment List

The equipment list is a file of equipment repair parts. The equipment list includes stocked and non-stocked parts.

As new equipment is added to the plant systems, or as additional repair part requirements are identified, the file is updated.

Parts Ordering

Parts are ordered as follows.

When a maintenance or repair requirement is added to the corrective maintenance work list, the parts requirements are evaluated and the spare parts stock is checked to verify part availability. If the parts required are not stocked on site, the parts are ordered and staged for the next available outage.

At the end of each area outage, the outage routine is used to generate a parts replacement order based on input from the personnel who performed the actual repairs.

The day to day maintenance activity is reported to the maintenance supervisor. This report includes any spare parts used to complete the repairs. The maintenance supervisor orders and stores the spare parts upon receipt.

Spare Farts inventor OM 3-03A	
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	Block House Block House Block House	900	Pole Barn	Pole Barn	Pole Barn		Block Building	Block Building Block House	Block House	Block House		Central SH F2	Sellia or 12	Central		Central SH L34	Central		Contral SH Lg	Central SH L17	Central SH L17				Central SH 1.11	Central srt L34	o de	Cernial Sri III						Central SH H2				Super, Locker	Central SH L34					Central SH H6	Central SH H6 Central SH H6					Central SH 117		518-235-1610 Supervisor Cabinel
	800-523-9482 800-523-9482 800-523-9482	800-523-9482	J92 800-227-8464 800-523-9482	900 800-227-8464	09; 800-227-8464	800-227-8464	518-272-4920	800-227-8464 800-523-9482	800-523-9482	800-523-9482 612-646-9631	100-010-010	518-427-5800		518-272-4920	318-272-4920		518-181-2244	518-383-2244				DOOR OFF DATE	518-272-4920	518-272-4920		518-383-2244	518-383-2244	716-344-3156	518-383-2244	518-383-2244	518-383-2244	518-383-2244		732-329-3200	518-383-2244	518-274-5091	518-383-2244 518-383-2244		717-832-8873		518-383-2244	518-383-2244	518-383-2244			518-423-2081	518-423-2081		918-835-7325 803-831-8253		800-876-5406	
	Used on 3-15/16" dia. (East) crosshead wheel shaft Used on 5" dia. (West) crosshead wheel shaft				Alloy HH (stainless), 25% Cr, 12% Ni, Euler #111-93-4-09; 800-227-8464	Standard Wear Plate, Fuller #111-54-2-0589-12 Standard Wear Plate, Fuller #111-54-2-0589-18	2-7/16" dia., 15-1/2" long, (4) 11/16" holes in-line			Uses lever P/N 111-54-3-0296-01 92-4439-1		Z required for full change		(1) required for operation	4 required for full change 16 oz Flint, 70/450, w/2WP0706PX Cap.		Malerial CD4M for Mark III 2K3+2-13	Material: CS, for Mark III 2K3x2-13		Hub; MO, 1 250 Bolh Sides, Insert, MO		Mr Hub P/N. 10588, Pp Hub P/N. 26875, Insert: LO75	Hubs unknown		Hubs Req'd: Pp = 1-1/8" & Mtr =1-5/8" w/3/8" KW	Malerial: CD4M, for Mark III 2K3x2-13	Material: CS, for Mark III 2K3x2-13		Teflon gasket	1-ivil gasket 1-7/8" shaft	1-7/8" shaft	13" terion gasket 13" teflon gasket	ace, 1/4" NPT/LM, Type 213,53	0-15 ps; 1 pst mervals, 0.5 ps; graduations, 4-1/2" face	Malerial: CD4M, for Mark III 2K3x2-13; 13" trim 518-383-2244 Malerial: (DCI) durdio rast iron for Mark III 2K7x2-13" 9 0" 1 518-383-2244	metric		4.5x5.75x0.625x0.625, 7 R/S, 1 SelfAgitator	62" per tank	Casting No. 12 0289 ML80	יע מיוחשט איז א אראב ארטט עפר ארטט איז ווא איז א 436117 SandPIPER preumatic diaphragm pump	347215 45 psi, minimum required at kilns	9220374 type HL80 375712(E).375711(W) No snecific pressure requirements	6" FOR Tank 200A Only, Use se	6" For Tanks 100A, 100B, 100C, 200B AND 200C 6" For Tanks 300, 400, 500 & 600 (Outside)	2-1/2 shaft size	1-7/8", Double Bellows Mechanical Seal 1-7/8", Old Reliable		641102181, Applied Process Technology	MAPA P/N 331 Both Yokes: 1/2" KW 1-1/4" Yoke P/N: 11/1552 1" Yoke P/N: 11/1524		K I Ft. body & Seals, 55 ball & stem, Steel WCB 150 1-1 1/2" F x 1/2" F, ball cone check valve
	111-30-5-6797-00 111-10-5-6947-03 111-10-5-6947-07	111-58-1-0346-01 TC5000-111	111-92-4-0900-90 Rev. 4	LE-55PC-1	LE-55PC-1R		170-33-8	111-62-2-0238-51	111-62-2-0237-50	111-54-3-0296-04 HWAC-115 HRS	LMLF-31T1-P31	53117U	NJ 314 ECM / C3	8M-896-62	1ERB161LN	SK x 48 mm	SF X 25:3/8 AT100, CD4M	AT100, CS	1.099 / L.160		L100 x 1,250	10 75 No. 41	No. 8U	No. 8J	L110 21 0552 0115	AS106D, CD4M	AS106D, CS	23,0586,9923	2Z190G	22.150	22104	AS107 AS107	9767061	J340K81 HA20SS250F	AT1030P AT103RV	M12 with 1,75 thread	2K201B 2Z131	14R-4500x63-7	23.0553.0111	12.0289.0115	SB1-A Type SB-4-A	2K3X2-13/126	0230 DP10 2K3X2-13/90	CDCV + BDI	Cat-Vac (MFG # 301029) ENV III (MFG # 314410	SMEC Liberator Seal	SMEC DDI Bellows 5E2Z3VH	16.0685,8821	20613-21G7A	Spicer P/N 5-176X	88-24A-01	62-103-01
	FFE Minerals FFE Minerals FFE Minerals	FFE Minerals Temperform Corp.	FFE Minerals	Temperform Corp. Temperform Corp.	Temperform Corp.	Temperform Corp.	FMC/Troy Belt	FFE Minerals	FFE Minerals	rrc minerals Industrial Air Systems	John Crane / Lemco	SKF Applied	SKF	Gates/Troy Belt	Birch Bottle	Kaman	Durco/Roffe Industries	Durco/Roffe Industries	Love Joy/Tray/Applied Love Joy/Tray / Applied	Alra-Fles	Lovejoy/Tray Belt	Lovedy/Applied SureFley/Tray Bett	SureFlexTroy Belt	SureFlex/Troy Belt	Love Joy/Troy / Applied Godwin	Durco/Rolfe Industries	Durco/Rolfe Industries	Godwin	Durco/Rolfe Industries	Durco/Rolfe Industries	Durco/Rolfe Industries	Durco/Rolfe Industries	Wika Instrument Corp.	wemaster-Carr Marwin	Durco/Rolfe Industries Durco/Rolfe Industries	Dougleas	Durco/Roife Industries Durco/Roife Industries	Chesterton Delindolable Misore	Godwin	Godwin Bahm Ind / Env Anner	Warren Rupp / Rolle Ind.	Durco/Rolfe Industries	Control/Rofe Industries	Confinental Disc	Confinental Disc	Frederick Seals	Frederick Seals Frederick Seals	Godwin	Mission Fluid King	Spicer/Albany Universal Chicago Rawhide	Apollo/Collins Pipe	Conbraco/Uncle Sam
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	Frame assy, cooler window air seal Packing, felt, cooler shall air seal, 3-16/16" Dia Packing, felt, cooler shall air seal, 5" Dia	Pin, shear, cooler driven sprocket Plate, grate, flat, universal, cast steef	Plate, grate, RFT (pocket), center, stainless	Plate, grate, rkr I (bocket), cemer, stainless Plate, grate, RFT (pocket), LH, stainless	Plate, grate, RFT (pocket), RH, stainless Plate side casting. I H kin confer past all	Plate, side casting, RH, kiln cooler, cast stl.	Shaft, coupling, Kiin cooler screw T-bott areamble Kiin cooler screw	Wheel assy, 3.5' bore, cooler wheel shaft	Wheel assy, 4.0° bore, cooler crosshead shaft Wickel cooler incredian window cover.	Air Handling Unit	Barrier Fluid Reservoir Bearing 1000 & 2000 Dumos	Bearing, Vacuum Pump	Bearing, Vacuum Pump	Beff, Cog, 100C & 200C pumps Beff, "V", Gear pump, Frac	Bottle, Sample	Bushing, Godwin Pump Bushim Vacuum Puma (Puma Sida)	Casing, impeller, FF lower pad pump	Casing, Impeller, FF waste oil pump	Coupling Insert, barret Augur Coupling Insert, Oil Unioading	Coupling, Barrel Augur Drive (Test)	Coupling, Hub. Barrel Augur Drive (Both Sides)	Coupling steers, FF Building Heating Pumps	Coupling steeve, FF lower pad pump	Coupling sleeve, FF waste oil pump	Coupling, Oil Officiality, port refless Cover, Inspection, Godwin Pumps	Cover, rear, FF lower pad pump	Cover, rear, FF waste oil pump Diaphragm, Air Pump (2*)	Filter, FF Godwin Unloading Pump Priming	Gasket, gland, FF lower pad pump Gasket, gland, FF waste oil numn	Gasket, impeller, FF lower pad pump	Gasket, impeller, FF waste oil pump Gasket, macrover, FF lower had nump	Gasket, rear cover, FF waste oil pump	Gauge, pressure, FF lower pad pump Gauge, pressure, FF outskip tank	Handle, Valve, Inside Tank	Impeller, FF lower pad pump Impeller, FF waste oil pump	Nut, FF Godwin Pumps	O-ing, Fr Lower Fao pumps bearing Camers O-ring, FF Lower Pad pumps Bearing Hsg Adapter	Packing, Agitator Packing stuffed how I GF leside tanks	Pin, Retaining, Godwin Pumps	Plate, backing, FF LGF Godwin pumps Pressurizing system FF Cabinal N2 Pume	Pump, Anti-freeze	Pump, Lower Pad, Outside Tk 300 - 600 Pump, Off-bad	Pump, Waste Oil	Rupture Disc, FF, Inside Tank 200A Only	Rupture Disc, FF, its de Tanks Rupture Disc, FF, Outside Tanks	Seal, FF Inside LGF pump Seal, FF tower nad numn	Seal, FF waste oil pump	Shaft, pump, FF LGF Godwin pumps Sintt Class FF Mission pump Raniar Fluid	Seeve assy, shaft, A & B pumps	Universal Joint, Barrel Augur Universal Joint, Barrel Augur	Vaive, ball, 4"-150# flanged, full port Vaive, ball, FF, 1-1/2" Flanced Ball recirculators	Valve, check, FF, Unloading Pump Närogen Prime
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STEGGOZZIV 12299SH-84736 Tight argue double reduction, 5GC frame 518-273-500 Pobe Barn	lndustries Pump Co./Grain;	2KZX2R-10/70 Cat. No. 50290	379776 Mark III Recessed Impeller Pump	518-383-2244				
FWC738 d00B5G	E Mineral	ST5050221V		518-273-1713 513-367-3121	Block Building		2	
1572.2 63EM12390002 67 PermanFib Feater 15717A-7301 610.6895-9700 1572.2 63EM12390002 67 PermanFib Feater 15717A-7301 610.6895-9700 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 125 pilets per seri [Min stock 300] 206.671-132 158.04.12 Approx 142 Appr	n/Applied	FWC738 400B5G		518-427-5800	Pole Barn	-		
SECURIOR Chemical Part Chemical Strict C		15721-2		610-695-9700			2	
DA 3.01042.94.320	istruction Prod.	5/8*-11 UNC x 1* king		518-458-1141				
SECOLE 1-187. OR Reliable 516-22-2081	Tech	DA 301042-84-320	Approx 125 plates per seal (Min stock 300)	205-621-4321	Central SH K 13 Central SH K8	250 27		
BY50424G Fired F	eals eals	5EBC4E 5E2Z3VH	1-1/8", Old Reliable 1-7/8", Old Reliable	518-423-2081				
9948 [WP-4] 9948 [WP-4] 995042D ALT NO. 22118 Impelies side, for Mark III 2RC22R-10 995042d S2CCISV From the Coupling side, for Mark III 2RC22R-10 995042d 1-7/16* shaft, Won O-ring MTD Ceramic Seat 518-423-2081 1-7/16* shaft, Won O-ring MTD Ceramic Seat 518-423-2081 1-7/16* shaft, Won O-ring MTD Ceramic Seat 518-423-2081 1-7/16* shaft, Won O-ring MTD Ceramic Seat 518-223-2081 1-7/16* shaft, Won O-ring MTD Ceramic Seat 518-22-2081 1-7/16* shaft, 19 move 10-22-2081 1-7/16* shaft, 10-22-2081	e Industries e Industries	BY50424G BY50424B	impeller side, for Mark III 2x2R-6 Coupling side, for Mark III 2x2R-6	518-383-2244 518-383-2244				
SECONDARY SIGNATURE STATE	aman	9848 (LWP-4) RV50424D		518-783-8114				
522C3V or 419187A4 1-178 shaft, Vion O-ring MTD Ceramic Seat 516-423-2801 10-23.284 1-178 shaft, Vion O-ring MTD Ceramic Seat 516-423-2801 10-23.284 10-23.2	a Industries	BY50424C BY50424C		518-383-2244				
100-30 11-68 shaft 516-273-1713 Central SH J 516-273-1773 Central SH J 516-273-1773 Central SH K8 516-273-2744 Central SH K8 516-273-1773 Central SH K8 516-273-1773 Central SH K8 516-273-2744 Central SH K8 516-273-1773 Central SH K8 516-273-2744 Central SH K8 516-2744 Centra	seats	5ZZC3V or 1419187AA	1-7/8 shaft, Viton O-ring MTD Ceramic Seat	518-423-2081				
1.1105 (318SS) Haleriat; 216 SS, for Mark III 2K2x2R-10, 1-718' dia, 516.383-2244 2.7105 - 2H Uses bushing SH, 1-510' staft, 3 gnove 516.427-5800 3.3V 4,12 SH Uses bushing SH, 10' staft, 3 gnove 516.427-5800 3.3V 4,2 SH Uses bushing SH, 10' staft, 3 gnove 516.427-5800 3.3V 4,2 SH Use SH x 1-710' Euclidig SDSx1-567 2.A.1864.0.SH Use SH x 1-710' Euclidig SDSx1-567 2.A.1864.0.SH Use SH x 1-710' Euclidig SDSx1-567 3.A.1864.0.SH Use SDSx1-567 3.A.1864.0.SH 3	pul a	B00-30	i <i>-7l</i> 5 shaft	518-383-2244 518-273-1713 518-273-1713 518-273-1713	Central SH J Central SH K8 Central SH K8	es ro	-	
3.0V 4.12 SH Uses bushing SH, 15.6° shaft, 3 gnove 3.3V 4.12 SH Uses bushing SH, 15.6° shaft, 3 gnove 3.3V 4.2 SH Uses bushing SH, 15.6° shaft, 3 gnove 3.4.3 Est Shaft, 3 gnove 1.4.5 Shaft, 3	Industries Industries	1J105 (316SS) 2Y105 - ZH	Material: 316 SS. for Mark III 2KZx2R-10. 1-7/8" dia.	518-383-2244)		
3/34 4.5 SDS Uses bushing SDSA*-186" 2A.1684, DSH Use SH x 1-1/16 Bushing 2A.1684, DSH Use SH x 1-1/16 Bushing 1572A, 6' PermarFb Feeder, 15777A-1301 Norfle SK-121697-01 12' x 12' x 3/16' High temp, glass-ceramin, 1292 deg, F	led Ind. Tech.	3 3V 4.12 SH	Uses bushing SH, 1-5/8" shaft, 3 groove	518-427-5800				
AAJBB4 (USH USS)	fied Ind Tech	3/3V 4.5 SDS	Usees bushing SDSxx-5/8*	518-427-5800				
15720A 6' PermaFfo Feeder, 1571A, 1301 Northe SK-121897-01 4.25' Dia, 114' thick, tempered glass (PyrexTM) 12' x 12' x 3/16' High temp. glass-ceramic, 1292 deg. F		2A3.684.0-SH 2A3.684.0-SH	Use SH x 1-1/8" Bushing Use SH x 1-7/16" Bushing				•	
odulokog	.	15720A Norfite SK-121897-01	6° Perma/Fio Feeder, 15717A-7301 4.25° Dia, 1/4 thick, tempered glass (PyrexTM)	518-272-7041				
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Used on 3-1516* dia, (East) crossbead wheel shaft Used on 3-1516* dia, (East) crossbead wheel shaft some of us call this 2"C channel, fise of right sides (2) required Used on 3-1516* dia, (East) crossbead wheel shaft Used on 5" dia, (West) crosshead wheel shaft I shall, it Seeth, 3"C of chain, chandrad fewyar) 1" shall, it Seeth, 3"G of chain, chandrad fewyar, to sreed 1"3"4" shall, if Seeth, 3"G of chain, chandrad fewyar, Uses Trapelode 3020, 2"10" shaft """ Use to increase speed of riday feeder 7"3"G shaft, 10 teeth, 3"G of chain, 3"16" teywary """ 1"" shaft, 10 teeth, 3"G of chain, 3"IG" teywary """ 1"" shaft, 10 teeth, 3"G of chain, 3"IG" teywary """ shaft, 10 teeth, 3"G of chain, 3"IG" teywary """ shaft, 10 teeth, 3"G of chain, 3"IG" teywary """ shaft, 10 teeth, 3"G of chain, 3"IG" teywary """ shaft, 10 teeth, 3"G of chain, 3"IG" teywary """ shaft, 10 teeth, 3"G of chain, 3"IG" teywary """ shaft, 2" shaft	1/2 Ton 2 C-POYC True Union 4 C-POYCUT, True Union 4 C-POYCUT, True Union Binnze Valve w/S Bail: female NPT Theoads both end Adapter MKG80 fanged, SS bail & stem, todyscal RTFE, Adapter MKG90 fanged, SS bail & stem, todyscal RTFE, Adapter MKG90 fanged, SS bail & stem, todyscal RTFE, Adapter MKG90 fanged, SS bail & stem, todyscal RTFE, Hard Chrome Bail Hard Chrome Bail 4 Fand Chrome Bail 6 Fold fort, threaded, bronze body, TFE packing 600 pps threaded, bronze body, TFE packing 600 pps threaded, full fort, RTFE seal EFDM finer & seal, polypropylere disc	### OF Permards Feeder, OAT Cheannoon	The SECMA21S 2. 1971b strail, 1 Both Med Duty, Insent #123364 PU37 = 40.10 P PU37 = 40.10 P PU38 = 40.10 P PU38 = 20.10 P PU38 = 2.71 F start P28-SCM.207 2. both base, 2.71 f start P28-SCM.207 2. Poth base, 2. Poth base, 2. Poth base, 2. Poth base, 2.
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518-272-4920 77) 518-272-4920 518-272-4920 cani 518-272-4920 1	518-427-5800 518-427-5800 518-427-5800	518-427-5800	518-383-2244 518-383-2244 518-383-2244 518-383-2244 518-427-5800 618-427-5900 618-427-3930		518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800 518-427-5800
24* 2-ply, 31fe* top, 11fe* bim, 22d#im, 29d* bing 518-272-4920 24* 2-ply, 31fe* top, 11fe* bim, 22d#im, 18f* bing (183* 77) 518-272-4920 24* 2-ply, 31fe* top, 11fe* bim, 22d#im, 18f* bing 24* 2-ply, 31fe* top, 11fe* bim, 12d#im, 18f* bing 24* 2-ply, 31fe* top, 11fe* bim, 15d# 13d* bing 23* 3-ply* tiff* top, 11d* bim, 15d# 13d* bing 23* 3-ply* tiff* top, 11d* comparison of the solution of the so	2-1/8 inch shaft OD TYPE 3/4' keyway OD TYPE 5/6' keyway	2-1/2' shaft 2 Inch shaft	2° pitch 13° long Replacement element PN JE-CA000 94077 Use Seal KR 1180710 Recommended spacing is 1/4* Motor Hitb Hot Borset Para-Rex, last changed on 11/1/97 COVER 110071 4.195* bore (motor) T hubs, 1×1/2 KW	Telbon design. 4 f.625* dia. x 144.75* long 000-821-2222 IARA PN 6598. One required for operation 516-232-2244 PN 6598. One required for operation 617-223-6830 AN 57-223-6830 AN 57-223-6	15 'OD x 4" Lig and 15 'OD x 12" Lig. Carbon Sheel 14" D x 26" L, 27/16" shaft, 46" pon of 15 D x 26" L, 27/16" shaft, 46" pon of 15 D x 26" L, 27/16" shaft, 46" pon of 15 D x 26" L, 27/16" shaft, 46" pon of 15 D x 26" with Lagging 6.27/16" x 46" AOL Shaft M.O. #93-066667-01 31,12.1 ratio, 150HP Service Rating, SF 2.07 pon 13.12.1 ratio, 150HP Service Rating, SF 2.07 pon 13.2.1 ratio, 160 HP Service Rating, SF 2.07 pon 13.3.1 ratio, 218 HP ig. 2012 RPM 17 x 1/4" blue closed cell sillione, Last P.O. 966016 SK 1-7/8 bushing, 1-7/16" shaft 2 gnove, 172" sq. KW SDS 1-7/16 bushing, 1-7/16" shaft 2 gnove Uses bushing 57 2-7/16; 2-7/16" shaft, 5 gnove Uses bushing 57 2-7/16; 2-7/16" shaft, 5 gnove Uses bushing 57 2-7/16; 2-7/16" shaft, 5 gnove
Winglood Win	SDX x 1-170 SDX x 2-140 SF x 2-14 E x 2-1416 F x 2-34 F x 2-36 SF x 2-36 SF x 2-37 SF x 2-3	3536 x 3-3/8 2012 x 2 2517 x 2 3020 x 2-7/16 2517 x 2-1/2 3020 x 2-7/16	2012 x 1-308 LL0400-C OSI 500 ANA31A 1180T 1180T10 PX 70 1100T10	2960302 23456-2 28456-2 2851-04 110460-7 10460-7 615-26-24 615-36-24 016-34 0160wm Mobile 634 Morown Mobile 634 Morown	TXT415AT 465A3-C 2040FZA64 31 43 1175WESA60 177WESA60 174T25AF 850 17500 8K 2 59 8.00 SK 2 59 8.00 SK 2 59 8.00 SK 2 59 8.00 SK 2 59 8.2 SSS 2 SS 8.00 SK 2 59 8.2 SSS 2 SS 8.00 SK 2 SS 8.2 SSS 3 SSS 8 8.00 SK 2 SS 8.2 SSS 5 SS
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All 283.6 GSD Uses bushing E 2-7/8, 2-7/8* shall, 5 groove All 289.6 GSD Uses bushing 1610 x 1-2/8* shall, 2 groove All 289.6 GSC Uses bushing E 2-3/8, 2-3/8* shall 2 groove Uses bushing E 2-3/8, 2-3/8* shall, 3 groove Uses bushing SF 2-3/8, 2-3/8* shall, 3 groove Uses bushing SK 2-3/16, 2-3/16* shall, 3 groove Uses bushing SK 2-3/16, 2-3/16* shall, 3 groove Uses bushing SK 2-3/16, 2-3/16* shall, 3 groove Uses bushing SK 1-3/16, 1-3/16* shall, 2 groove Use bushing SK 1-3/16*, 1-3/18* shall, 2 groove	Use State of	THE Land Cates, 7.1.7 - par cate, 10.7 -	Each bearing uses (2) SKF seals Power Each Park 15th 5th 5th 5th 5th 5th 5th 5th 5th 5th	to required to the charge Trequired for the	****
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	N	,		1 complete set		72+	4 1 00 0	×		36	2 each 2
	Central SH L10	Central SH L7		Central SH L Central SH L17 Central SH L17 Central SH L17	Gemial SH L17	Block Building	Block House Block House	BACK HUDSO		Central SH L21 Pole Barn Central SH L23 Central SH L23	Tent Garage Tent Garage
	518-427-5800 518-427-5800 518-427-5800		518-383-2244	516-383-2244	518/427/5800 se 518-383-2244 518-272-4920 518-383-2244 518-383-2244	800-821-2222 518-383-2244	518-782-7180 518-383-2244 518-383-2244	518-353-2244 518-352-2244 518-427-5800 518-427-5800 518-272-4920 518-383-2244 518-383-2244	518-272-4920	518-427-5800 518-272-4920 518-785-8597	518-383-2244 518-383-2244
	2-18 Inch shaft OD TYPE 5/6* keyway OD TYPE 5/6* keyway		Replacement element P/N JE-C0600 D9188U89B nnan	JUBBI 7/18* bore motor sele. 1-3/0f* reducer site 7/16* bore metor site, 1-3/0f* reducer side For 1/175 Omnbox Reducer For 1/175 Omnbox Reducer	Seal for 3" Pine Coupling, ploing between compressor & se 519.427/5050 1.30° & 1-50° 1040T hubs 70° 10° anotor shaft 2.0° dia, reducer shaft 93.1-6189 93.1-6189 11° 50 milbox Reducer 518.339.2244 4899042739	metal bowl guard, 3/4" female NPT. Recuires filter element No. 811E	2 required. NAPA PIN 0369 Napa PIN 6795 MAPA PIN 8795	RAPIN 16 5:90 Replacement dement PIN JE-F0800 187W, 75 can, reg 2 backet PIN MD (DL 195700 187W, x 35 deg., 5° can 247W, x 35 deg., 5° can 247W, x 35 deg., 5° can	1-116 T PT I-LUGiaphine. Applox 50 per seal required 16 T D x 25 L, 2-7116 shaft, lagged 299031 RY 1-316 fingt shaft Uses a 145T Motor Bracket Uses a 145T Motor Bracket	5069492001DA 57.7*1 helical in-line reducer, 140TC frame 82 Degree Shoulder Used with Spher roller bearing 22244YMW33 16.0 x 18 0 x 0.780, 25003-5116	Also requires secondary separator P/N 122117-3 Also requires primary separator P/N 22715-3
807-1 x 710.2 807-1 x 10.2 807-1 x 10.2 807-1 x 10.2 807-1 x 10.2 807-1 x 20.2 807-1 x 20.2 807-1 x 20.2 807-1 x 20.2 807-1 x 20.2	3020 x 2-118 3020 x 2-118 3020 x 2-18 3020 x 2-18 5251 x 2-318 5251 x 2-318 5251 x 1-18 5251 x 1-18 5251 x 1-18 5251 x 1-18 537 x 1-18 538 x 2-118 538 x 2-118	F x 3-5/8 1 v 4 2012 x 2 2517 x 2 3020 x 2-7/16 2517 x 2	3020 x 2-7/16 JL0600-C SSR-EP100 OSL400 ANN3	103(IT Gref / phr 0782811 103(IT Gref / phr 0782811 1040110 1040110 4705615	E3D 121824 1040T10 4705615 TW4500 PS370-48P	2981689 25361-010 F25241-110 811	39703466 6343 23458-3	162952 215-16 BD-0120 205-16 BD-0120 205-16 BD-0120 203592-4 C33592-4 AV6-RA AV6-RA 340E	Style 1760 TP7720 DGR-2 2040F234-57.62:1 TA74254.7		22705-3
	Marin/Applied Ind. Tech. Marin/Applied Ind. Tech. Marin/Applied Ind. Tech.	Troy Bed Troy Red Dodge/Applied Ind. Tech.	Martin/Applied Ind. Tech. AIRTEK/Rolfe Industries ingersoll-Rand Onincy/Rolfe Industries	CulincyNation industries CulincyNation Falk Falk FalkTry Bell / Applied Falk/Try Bell / Applied Falk/Applied Falk/Applied	Omega/Applied Quincy/Rolfe Industries Quellay/Rolfe Ind. Tech. Falk/Applied Ind. AIRTEK/Rolfe Industries Defect/NAC Engineering	BHA ARO/Shako ARO/Shako Dettech/Roffe Ind.	Ingersoll-Rand/A/C Eng. NAPA Ouincy/Rolte Industries Ouincy/Rolte Industries	Olmsyword retastives ARTEKRottle industries ARApplied Ind. Tech. SAApplied to Smith FMCTroy Bet FMCTroy Bet FMCTroy Bet AquamaticRottle ind. AquamaticRottle ind. AquamaticRottle ind.	Troy Betting Airtech/Rolfe ind Dodge/Applied fnd. Tech. Dodge/Applied fnd. Tech. Dodge/Applied/Troy Bett Dodge/Applied/Troy Bett Dodge/Applied/Troy Bett Dodge/Art/ASAT	Falk Omnibox Dodge/Applied Ind Tech. Douglass SKF Garlock/Applied Ind Tech ARO/Shako	Quincy/Rolfe Industries Quincy/Rolfe Industries

Bushing Namional Reducts Shakes Bushing Hold Drine. Reducts Shakes Bushing, Screw, Cooler (North), Drive Spracket Bushing, Screw, Cooler (North), Drive Spracket Bushing, Screw, Cooler (North), Drive Spracket Coupley, Screw, Cooler (South), Drive Spracket Compressor, air, KD duling, Spracket Compressor, air, KD duling, Coupling (A. Mullacher Arieland) Coupling, Cooler Screw, (North & South) Coupling, Cooler Screw, (North & South) Coupling, Cooler Screw (North) Coupling, Cooler Screw (North) Coupling, Date Store (North) Coupling, Air Compressor, Outnery Coupling, Air Compressor, Outnery Coupling, Air Compressor, Outnery Coupling, XT sto Stake belt, head pulley Coupling, XT sto stake belt, head pulley Coupling, XT and compressor, Chinack Dryer, air XE and compressor, Africk Dryer, air XE all compressor, Africk Filter air, Camera Purp Air Filter air, Camera Purp Air NEICVP1120E01

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Norlite, LLC Cohoes, New York

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An up-to-date list is available from the maintenance manager.

Impeller, WW OFC pump Kit, spare parts, WW bleach pump, large Kit, spare parts, WW bleach pump, small

Balt, check, inon pump Balt, check, studge pump Balt, check, studge pump Bearing, Efflerent pump, outloant Beb. Cog, Polymer pump Bearing, Efflerent pump, outloant Bear, V. A. Compressor Bearb, Efflerent freatment Castin, impeller, WW efflerent pump Chamber, mixen, WW polymer Compressor, nie WW obert Compressor, nie WW obert Coupling, WW offer pump Coupling, WW offer pump Coupling, WW offer pump Coupling, WW offer pump Diaptragm, WW for pump Coupling, WW offer pump Diaptragm, WW to pump Coupling, WW offer pump Diaptragm, WW to pump Caster, sock, WW sock filters, 100 mesh Filter, KM Compressor, Culissey OT-25 Filter, Sock, WW sock filters, 100 mesh Filteriffeguleru WW, Item Sulfate Pump Gasset, gland, WW En pump Gasset, impeler, WW En pump Gasset, impeler, WW En pump Gasset, impeler, WW En pump

Mor	DA-2	56363-3 & 56363-4 2 hp. Air motor rebuilding kit - Gast Mfg. Com. K208	800-335-4981
ladelphia Mixers	PV-4 PTO	95SDJ0300 Order # 14744	717-832-8873
ladelphla Mixers	PV-4 PTO	95SDJ0301 Order # 14744	717-832-8873
ładelphia Mixers	PV-4 PTO	95SDJ0299 Order# 14744	717-832-8873
ladelphia Mixers	PV4 PT0	95SDJ0298 Order # 14744	717-832-8873
co/Rolfe Industries	1Y201B		518-383-2244
aare D/Grainger	9013FHG52J59X	STK NO. 2DC09	518-869-1414
anco	K2343002		800-882-6466
anco	7071001	12 teeth, 3/8" bore, set screw, aluminum	800-882-6466
anco	7071201	32 teeth, 3/8" bore, aluminum	800-882-6466
co/Rolfe Industries	E1-16138-68A54	EVO3311 Head kii #61-76-0123-PP2, plunger kii #61760160, head as 518-383-2244	as 518-383-2244
/Rolfe Indutries	L122-44	960910587 Uses spare parts kit P/N SP-44	518-383-2244
/Rolfe Indutries	A181-95S	92046763 Uses spare parts kit P/N SP-U1;18 GPD, 80 psi	518-383-2244
/Rolfe Indutries	A181-95S	930908614 Uses spare parts kit P/N SP-U1;18 GPD, 80 psi	518-383-2244
co/Rolfe Industries	E1-16076-62A34	EV03312 Head kit #61-76-0123-SS1, plunger kit #61760160, head at 518-383-2244	as 518-383-2244
co/Raife Industries	1K3x1.5-82RV/76	413155 & 413156 Mark III, P.O. #954257-00, EQ. # PC4629A & B	518-383-2244
co/Rolfe Industries	1K1.5X1-62 RV/37	413154 & 413153 Mark III, P.O. # -00, EO. # PC A & B 35 gpm	518-383-2244
rren Rupp / Rolfe Ind.	SB1-A Type SB-4-A		518-383-2244
co/Roffe Industries	1K1,5X1-82 RV/62	413825 & 413157 Mark III, P.O. #954257-00, EQ. # PC-4624A & B	518-383-2244
co/Rolfe Industries	1K3x1.5-62RV	Mark III	518-383-2244
men Rupp / Rolfe Ind.	EB2-M	489284 SandPIPER pneumatic diaphragm pump	518-383-2244
men Rupp / Rolfe Ind.	031-060-000	Used on SandPIPER SB1-A Type SB-4-A	518-383-2244
rren Rupp / Rolfe Ind.	476-100-000	For SandPIPER EB-2-M pump, includes pilot valve kit	518-383-2244
men Rupp / Rolfe Ind.	031-055-000	For SandPIPER EB-2-M pump, included in air end kit	518-383-2244
renson/ A/C Eng.	WK-R30-08-G00	0-120 psig out, 300 psig max in, 1" female in/out	518-371-4401
derick Seals	\$MEC105466	1-3/8", Tg Carbide rotary/Si Carbide O-ring seat	518-423-2081
derick Seals	\$MEC122543	1-3/8", Tg Carbide rotary/Si Carbide O-ring seat	518-423-2081
derick Seals	SMEC104500A	1-3/8", Viton carbon rotary/ SC O-ring seat	518-423-2081
теп Rupp / Raife Ind.	722-026-580	2 required on SandPIPER SB1-A Type 4, Buna N	518-383-2244
rren Rupp / Rolfe Ind.	722-040-365	4 required on SandPIPER EB2-M, reoprere rubber	518-383-2244
Master-Carr	5233K71	Clear, flexible PVC tubing, 3/4" ID x 1.0" OD	732-329-3200
/Roffe Industries	28022	Used on LMI model A181-95S metering pump	518-383-2244
ars/Uncle Sam		2-1/2" PVC, EPDM seal	518-235-1610
Hyd. Eng./Alb. Hyd.	20-4001A100		518-462-5425
gren/Filtration Systems	Norgren P/N 375-02-081-44		

ΙE	Mixer, pneumatic, WW fron sulfate	ww	MixMor	
ΞI	Mixer, WW EO tank	ww	Philadelphia Mixers	F/Ad
C	Mixer, WW EQ tank	ww	Philadelphia Mixers	P-Ad
VI	Mixer, WW overflow collection tank	MM	Philadelphia Mixers	77/10
o -	Mixer, WW studge tank	MM	Philadelphia Mivers	7/6
11	O-ring, WW pumps Bearing Carriers	MM	Durco/Bolfe Industries	
2	Pressure Switch / unloader, WW Quincey air comp	ww	Square D/Grainner	9013FHG52
01	Priming accessory kit, WW polymer mixer	ww	Strance	KC3K
ΞC	Pulley, WW polymer mixer, drive	ww	Stranco	707
)1	Pulley, WW polymer mixer, driven	ww	Stranco	707
	Pump, Acid Metering	ww	Durco/Rolfe Industries	E1-16138-6
	Pump, Bleach Metering, Backup (large)	ww	LMI/Rolfe Indutries	=======================================
	Pump, Bleach Metering, Primary (small)	ww	LMI/Roffe Indutries	A18
	Pump, Bleach Metering, Primary (small)	ww	LMI/Rolfe Indutries	A18
	Pump, Caustic Metering	ww	Durco/Rolfe Industries	E1-16076-6
	Pump, Effluent	ww	Durco/Rolfe Industries	1K3x1,5-82F
	Pump, Equalization	ww	Durco/Roffe Industries	1K1.5X1-62 F
	Pump, Iron Sulfate	ww	Warren Rupp / Rolfe Ind.	SB1-A Type SI
	Pump, Over Flow Collection	ww	Durco/Roffe Industries	1K1.5X1-82 F
	Pump, QW Clean Water	ww	Durco/Rolfe Industries	1K3x1,5-
	Pump, Sludge	ww	Warren Rupp / Roffe Ind.	ш
	Rebuild kit, WW fron pump pilot valve	ww	Warren Rupp / Rolfe Ind.	031-06
	Rebuild kit, WW sludge pump air end	ww	Warren Rupp / Rolfe Ind.	476-10
	Rebuild kit, WW sludge pump pilot valve	ww	Warren Rupp / Rolfe Ind.	031-05
	Regulator, pressure, WW air compressor	ww	Wilkerson/ A/C Eng.	WK-R30-08
	Seal, WW Eff. pump	ww	Frederick Seals	\$MEC10
	Seal, WW EQ pump	ww	Frederick Seals	\$MEC12
	Seal, WW overflow collection pump	ww	Frederick Seals	SMEC104
	Seat, ball check, WW iron pump	WW	Warren Rupp / Roife Ind.	722-020
	Seat, ball check, WW sludge pump	ww	Warren Rupp / Rolfe Ind.	722-04(
	Sight tube, WW HCL tank	ww	McMaster-Carr	523
	Vaive, 4 function, WW small bleach pump	ww	LMI/Roffe Industries	2
	Valve, bail, WW Effluerd	ww	Spears/Uncle Sam	
	Valve, pressure release, WW filter press	ww	SC Hyd. Eng./Alb. Hyd.	20-4001
A	Valve, selector, WW Filter Press	ww	Norgren/Filtration Systems	Norgren P/N 375-02-08
p	Tubing, PVC, 3/4"	WWTP	Applied	
p	Tuhim PVC. 1*	TANATED	Applied	1404



Policy Number: OM 3-04

Effective Date: 9/03

PERFORMING DAILY, WEEKLY AND MONTHLY CALIBRATIONS

I. PURPOSE

Provide a consistent and reliable procedure for the daily, weekly and monthly calibration of emissions equipment.

II. SCOPE

Continuous Emissions Monitoring Equipment

III. RESONSIBILITIES

Instrumentation and Electrical Department

IV. PROCEDURES

See SOP's OM 3-07A thru OM 3-07I for procedures on how to perform calibrations.

See attachment OM 3-04A for the frequency of calibrations performed on each piece of equipment.

The Relative Accuracy Test Audits (RATA's) will be performed during the First Quarter of each year.

The quarterly Cylinder Gas Audits (CGA's) will be performed during the Second, Third and Fourth Quarter's of each year.



NORLITE CORPORATON
Policy Number: OM 3-05

Effective Date: 9/03

INSTRUMENT TAG NUMBERS

I. PURPOSE

Provide a list of instrument tag numbers.

II. SCOPE

Instrumentation Tags

III. RESONSIBILITIES

Instrumentation and Electrical Department

IV. PROCEDURES

Refer to Attachment OM 3-04A for list of instrument tag numbers.



NORLITE CORPORATON Policy Number: OM 3-06

Effective Date: 9/03

PREVENTIVE MAINTENANCE-EMISSIONS EQUIPMENT

I. PURPOSE

Provide a consistent and reliable procedure on and when preventive maintenance is done on emission equipment.

II. SCOPE

Preventive Maintenance of Emissions Equipment

III. RESONSIBILITIES

Instrumentation and Electrical Department

IV. PROCEDURES

Preventive maintenance (pm's) is performed monthly and during planned kiln shutdowns. PM's will be completed on the following components.

Pressure Taps

The pressure taps are to be cleaned by reaming the inside of the tube out and making sure it is clear of material buildup or debris.

Drives

Clean the drives using a nitrogen blowout system.

<u>Filters</u>

Clean the filters by blowing them with air, rinse them off or replace them, depending on their condition.

Flowmeters

Flowmeters will be cleaned using a 50% HCL solution. Scrub the inside of the flowmeter with the solution until clean.

Scrubbers

Refer to Norlite Corporation Best Management Practices Plan (BMP), Appendix F, 2.3.4 for procedures.

Plugged Line

Take line out of service and flush line and fitting with solution of Acetic Acid. After Acetic Acid, rinse with water and replace parts. Place line back into service.



Policy Number: OM 3-07A

Effective Date: 9/03 Revised: 10/03

LOW PRESSURE CALIBRATION

I. PURPOSE

Provide a consistent and reliable procedure for the calibration of equipment for Low Pressure settings. (instrument calibrated in inches of water)

II. SCOPE

Continuous Monitoring Systems

III. RESPONSIBILITIES

Instrumentation and Electrical Department

- 1. Attach communication device to transmitter.
- 2. Close isolation valves.
- 3. Attach pump and pressure calibrator to Hi side of pressure sensor.
- 4. Open Lo side of pressure sensor.
- 5. Open pump valve to check zero-take readings from communication device.
- 6. Close pump valve and pup up pressure to ½ upper range value-take readings.
- 7. Pump pressure to ½ upper range value-take readings.
- 8. Pump pressure to ¾ upper range value-take readings.
- 9. Pump pressure to upper range value-take readings.
- 10. If readings are out of drift, adjust transmitter to pressure calibrator readings.
- 11. Put equipment back to normal operating condition.



Policy Number: OM 3-07B

Effective Date: 9/03 Revised: 10/03

HIGH PRESSURE CALIBRATION

I. PURPOSE

Provide a consistent and reliable procedure for the calibration of equipment for High Pressure settings. (instrument calibrated in pounds per square inch)

II. SCOPE

Continuous Monitoring Systems

III. RESPONSIBILITIES

Instrumentation and Electrical Department

- 1. Attach communication device to transmitter.
- 2. Close isolation valves.
- 3. Attach pump and pressure calibrator to Hi side of pressure sensor.
- 4. Open pump valve to check zero-take readings from communication device.
- 5. Close pump valve and pump up pressure to ¼ upper range valve-take readings.
- 6. Pump pressure to ½ upper range value-take readings.
- 7. Pump pressure to ³/₄ upper range value-take readings.
- 8. Pump pressure to upper range value-take readings.
- 9. If readings are out of drift, adjust transmitter to pressure calibrator readings.
- 10. Put equipment back to normal operating condition.



Policy Number: OM 3-07C

Effective Date: 9/03

TEMPERATURE THERMOCOUPLE CALIBRATION

Revised: 10/03

I. **PURPOSE**

Provide a consistent and reliable procedure for the calibration of equipment for Temperature Thermocouple settings.

II. **SCOPE**

Continuous Monitoring Systems

III. RESPONSIBILITIES

Instrumentation and Electrical Department

- 1. Attach communication device to transmitter.
- 2. Take sensor wires off transmitter and attach wires from temperature simulator in their place.
- 3. Dial in Low range value on temperature simulator-take readings from communications device.
- 4. Dial in value ¼ of upper range value-take readings.
- 5. Dial in value ½ of upper range value-take readings.
- 6. Dial in value ¾ of upper range value-take readings.
- 7. Dial in upper range value-take readings.
- 8. Adjust transmitter if necessary.
- 9. Put equipment back to normal operating condition.



NORLITE CORPORATON
Policy Number: OM 3-07D

Effective Date: 9/03 Revised: 10/03

SCRUBBER FLOW CALIBRATION

I. PURPOSE

Provide a consistent and reliable procedure for the calibration of equipment for Scrubber Flow settings.

II. SCOPE

Continuous Monitoring Systems

III. RESPONSIBILITIES

Instrumentation and Electrical Department

- 1. Remove transmitter cover.
- 2. Unplug transmitter power and communication ribbon connector.
- 3. Attach simulator ribbon connector and power plug from simulator.
- 4. Plug in simulator to outlet power.
- 5. Dial simulator to Low range signal-take readings from amp meter and transmitter.
- 6. Dial in signal ¼ of upper range value-take readings.
- 7. Dial in signal ½ of upper range value-take readings.
- 8. Dial in signal ³/₄ of upper range value-take readings.
- 9. Dial in signal for upper range value-take readings.
- 10. If readings are out of drift, adjust transmitter to simulator signal reading.
- 11. Put equipment back to normal operating conditions.



Policy Number: OM 3-07E

Effective Date: 9/03 Revised: 10/03

INDUCED DRAFT FAN CURRENT CALIBRATION

I. PURPOSE

Provide a consistent and reliable procedure for the calibration of equipment for Induced Draft (ID) Fan Current settings.

II. SCOPE

Continuous Monitoring Systems

III. RESPONSIBILITIES

Instrumentation and Electrical Department

- 1. Clamp amp clamp around each drive output wire-take readings.
- 2. Take amp reading from control room computer.



NORLITE CORPORATON
Policy Number: OM 3-07F

Effective Date: 9/03 Revised: 10/03

FLOWS (MICROMOTION) CALIBRATION

I. PURPOSE

Provide a consistent and reliable procedure for the calibration of equipment for Flows (Micromotion) settings.

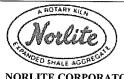
II. SCOPE

Continuous Monitoring Systems

III. RESPONSIBILITIES

Instrumentation and Electrical Department

- 1. Attach communication device to transmitter.
- 2. Change output reading from gallons per minute to pounds per minute.
- 3. Zero the totalizer.
- 4. Weigh bucket for tare weight.
- 5. Take sample in the basket and weigh-write down reading.
- 6. Write down totalizer reading form communication device and zero totalizer.
- 7. Take three samples and average.
- 8. If sample average and totalizer average is out of drift-redo test.
- 9. Put equipment back to normal operating condition.



NORLITE CORPORATON
Policy Number: OM 3-07G

Effective Date: 9/03

Revised: 10/03

DAILY pH (SCRUBBER) CALIBRATION

I. PURPOSE

Provide a consistent and reliable procedure for the calibration of equipment for Daily pH (Scrubber) settings.

II. SCOPE

Continuous Monitoring Systems

III. RESPONSIBILITIES

Instrumentation and Electrical Department

- 1. Calibrate hand held pH tester.
- 2. Clean pH probes with acid.
- 3. Take sample of scrubber water and test with hand held tester.
- 4. Check reading against transmitter reading.
- 5. If readings are out of drift, attach communication device to the transmitter and standardize.
- 6. Two point calibrate if a new probe is installed.



Policy Number: OM 3-07H

Effective Date: 9/03

Revised: 10/03

SHALE FEED CALIBRATION

I. PURPOSE

Provide a consistent and reliable procedure for the calibration of equipment for Shale Feed settings.

II. SCOPE

Continuous Monitoring Systems

III. RESPONSIBILITIES

Instrumentation and Electrical Department

- 1. Close silo plate to shut off shale feed and auto zero feeder.
- 2. Weigh buckets for tare weight.
- 3. Calculate belt speed by averaging three tachometer readings.
- 4. Open silo plate.
- 5. Take three shale sample grabs and average the weights.
- 6. Calculate the tons per hour and compare this to the current shale set point.
- 7. If the readings are not within drift, adjust the feeder and take two more sample grabs.
- 8. Put equipment back to normal operating condition.



NORLITE CORPORATION
Policy Number: OM 3-07I

Effective Date: 9/03 Revised: 10/03

LIME FEEDER CALIBRATION

I. PURPOSE

Provide a consistent and reliable procedure for the calibration of equipment for Lime Feeder settings.

II. SCOPE

Continuous Monitoring Systems

III. RESPONSIBILITIES

Instrumentation and Electrical Department

- 1. Run feeder at designated setting.
- 2. Measure revolutions per minute of Helix drive shaft.
- 3. Calculate output of feeder.
- 4. Compare output of feeder to target weight-if outside drift, adjust drive speed.
- 5. Put equipment back to normal operating condition.



Policy Number: OM 3-07J

Effective Date: 9/03

Revised: 10/03

SCRUBBER TANK LEVEL

I. PURPOSE

Provide a consistent and reliable procedure for the calibration of equipment for Scrubber Tank Level settings.

II. SCOPE

Continuous Monitoring Systems

III. RESONSIBILITIES

Instrumentation and Electrical Department

- 1. Attach communication device to transmitter.
- 2. Close isolation valves.
- 3. Open drain valve to Hi side of pressure sensor: make sure all fluid drains.
- 4. Close drain valve to Hi side of pressure sensor.
- 5. Attach pump and pressure calibrator to Hi side of pressure sensor.
- 6. Open Lo side of pressure sensor (if you are looking at a differential pressure)
- 7. Open pump valve to check zero-take readings from communication device.
- 8. Close pump valve and pup up pressure to ¼ upper range value-take readings.
- 9. Pump pressure to ½ upper range value-take readings.
- 10. Pump pressure to ¾ upper range value-take readings.
- 11. Pump pressure to upper range value-take readings.
- 12. If reading are out of tolerance, adjust transmitter to pressure calibrator readings.
- 13. Put equipment back to normal operating condition.
- 14. See Attachment OM 3-04B for the operational and waste feed cut criteria.



Policy Number: OM 3-07K

Effective Date: 9/03

CONTINUOUS EMISSIONS MONITORING SYSTEM-CALIBRATION

I. PURPOSE

Provide a procedure for the calibration of the Continuous Emissions Monitoring System (CEMS).

II. SCOPE

Continuous Emissions Monitoring Systems

III. RESPONSIBILLITIES

Instrumentation and Electrical Personnel (I & E)

IV. PROCEDURE

Calibration for CO-Low

- 1. Press and hold the blue CO-Low button on selected unit for 5 seconds. (The unit will automatically zero and span its self.)
- 2. Adjust the analyzer as necessary.
- 3. When the calibration is finished print out results.

Calibration for CO-Hi

- 1. Press and hold the blue CO-High button on selected unit for 5 seconds. (The unit will automatically zero and span its self.)
- 2. Adjust the analyzer as necessary.
- 3. When the calibration is finished print out the results.

Calibration for Oxygen

- 1. Press and hold blue Oxygen button on selected unit for 5 seconds. (The unit will automatically zero and span its self.
- 2. Adjust the analyzer as necessary.
- 3. When the calibration is finished print out the results.



Policy Number: OM 3-07L

Effective Date: 9/03

CONTINUOUS EMISSIONS MONITORING SYSTEM-LINEARITY TEST

I. PURPOSE

Provide a procedure for the linearity test of the Continuous Emissions Monitoring System (CEMS).

II. SCOPE

Continuous Emissions Monitoring Systems

III. RESPONSIBILLITIES

Instrumentation and Electrical Personnel (I & E)

IV. PROCEDURE

- 1. Perform Daily 24 Hour Cal Check.
- Check Pressures and Flows for CEMS.
- Perform online calibration for the analyzer. Zero and Span to Cal Values if needed.
- 4. Check DARS. Audit field for 20 second time period.
- 5. Connect audit gas equipment.
- 6. Record gas cylinder information on data sheet: EPA Protocol Gas, Cal Values, Expiration Date and Pressures.
- Call Kiln Control Room and notify CEMS is to be placed OUT OF SERVICE for Audit.
- 8. Place CEM OUT OF SERVICE.
- 9. Connect Outlet of Audit Gas Cylinder to outlet of Cal Line going to the probe.
- 10. Start Audit for DARS (Audit Button), (On Screen Lower Right0.
- 11. Perform 3 Audit runs as follows:

Run 1. LOW, MID, HIGH (Check analyzers to see if

you have enough gas)

Run 2. MID, LOW HIGH

Run 3. LOW, MID, HIGH

- 12. Open 1st Gas Cylinder and flow gas (10 lpm) wait until readings become stable on the Analyzer and DARS. Check Audit results for pass/fail limits (1st Run).
- 13. Let reading stabilize for 1 minute, Start 2nd Audit Gas, Repeat Step 12.
- 14. Let reading stabilize for 1 minute, Start 3rd Audit Gas, Repeat Step 12.
- 15. Perform Run 2 Repeat Steps 12 15.
- 16. Perform Run 3 Repeat Steps 12 15.
- 17. Stop Audit when readings return to normal. Print and record data for each run on the Field Data Sheet.
- 18. If CEMS Passes Linearity Test, disconnect audit equipment, reconnect Cal gas line to CEMS and flow Zero Gas (Blue Button) for 3 minutes. Check for leaks, analyzer should have a stable zero reading.
- 19. Place CEMS back into SERVICE, Record events in CEMS Log Book. Contact Kiln Control Room.
- 20. Backup Audit file by: COPYING Audit file from CEDAR to removable zip drive.

NORLITE CALIBRATION ERROR DATA SHEET

SOURCE:	NORLITE CORP.		DATE:
MONITOR:			LOCATION:
SERIAL NUMBE	R:		TIME:
		ANALYZER I	RANGE:
CYLINDER	LOW	MID	HIGH
TANK I.D. #		aki ngi ngungungan ngunggan kang ngungungan ngung ngunggan ngunggan ngunggan ngunggan ngunggan ngunggan ngung	
EXPIRATION			
TANK PSI			

RUN	CALIBRATION	MONITOR		DIFFERENCE	
NUMBER VALUE		RESPONSE	LOW	MID	HIGH
1-LOW					
2-MID					
3-HIGH					
4-MID		STANDARD TO STANDA			
5-LOW					
6-HIGH		·			
7-LOW					
8-MID		•			
9-HIGH					
		MEAN DIFF.			·
		CAL. ERROR*			

AUDIT POINTS	LOW	MID	HIGH
	0-20%	30-40%	70-80%
СО			
LOW (200 ppm)	0-40 ppm	60-80 ppm	140-160 ppm
HIGH (3000ppm)	0-600 ppm	900-1200 ppm	2100-2400 ppm
OXYEN (25%)	0-2%	8-10%	14-16%

* CAL. ERROR SPECIFICATION	MEAN DIFF.	
CO ANALIZER = <5% SPAN CAL. ERR =		X 100
LOW = 10 ppm HIGH = 150 ppm	RANGE	
OXYGEN ANALIZER = 0.5%		



Policy Number: OM 3-07M

Effective Date: 6/04

Revision Date: 1/05, 2/05

STACK GAS FLOW METER

I. PURPOSE

Provide a consistent and reliable procedure for the Stack Gas Flow Meter.

II. SCOPE

Stack Gas Flow Meter

III. RESPONSIBIILITIES

Compliance/I & E Department

IV. PROCEDURE

MONTHLY

- 1. The Stack Gas Flow Meter will be visually inspected each month.
 - a. Visually inspect electrical connections, enclosures, electrical cables and the flow element mounting connections for any signs of physical damage and/or deterioration.
 - b. Compare readings from control room to reading in field.

QUARTERLY

- 1. Each quarter the stack probe will be removed from the stack and cleaned.
 - a. Remove stack probe and clean.
 - b. Look for any signs of damage and/or deterioration.

ANNUAL

- 1. A RATA will be conducted on an annual basis for certification.
 - a. Certify instrument is in compliance.

NORLITE CORPORATION INSTRUMENT CALIBRATION DATA SHEET

NAME: STACK GAS FLOW METER KILN #1
MFG: FCI
MODEL#: GF90
SERIAL#: 244110A
CERT. DUE: 11/05
TAG#: FT-5555
LOCATION: KILN 1 MCC
METER READING FIELD:
METER READING CONTROL ROOM:
METER READING DIFFERENCE:
VISUAL INSPECTION (STACK):
VISUAL INSPECTION (ELECTRONICS):
DATE:
INSTRUMENT TECHNICIAN:
DRIFT ACCEPTANCE +/- 5%
COMMENTS:
QUARTERLY CLEANINGS:
MARCH
JUNE
SEPTEMBER
OLI ILIVIDLI(
DECEMBER

NORLITE CORPORATION INSTRUMENT CALIBRATION DATA SHEET

NAME: STACK GAS FLOW METER KILN #2
NAME. STACK GAS FLOW METER KILN #2
MFG: FCI
MODEL#: GF90
SERIAL#: 246163
CERT. DUE: 11/05
TAG#: FT-5555
LOCATION: KILN 2 MCC
METER READING FIELD:
METER READING CONTROL ROOM:
METER READING DIFFERENCE:
VISUAL INSPECTION (STACK):
VISUAL INSPECTION (ELECTRONICS):
DATE:
INSTRUMENT TECHNICIAN:
WOTHOWEN TESTINOTIVE
DRIFT ACCEPTANCE +/- 5%
DRIFT ACCEPTANCE +/- 5%
DRIFT ACCEPTANCE +/- 5% COMMENTS:
DRIFT ACCEPTANCE +/- 5% COMMENTS: QUARTERLY CLEANINGS:
DRIFT ACCEPTANCE +/- 5% COMMENTS: QUARTERLY CLEANINGS: MARCH
DRIFT ACCEPTANCE +/- 5% COMMENTS: QUARTERLY CLEANINGS: MARCH JUNE
DRIFT ACCEPTANCE +/- 5% COMMENTS: QUARTERLY CLEANINGS: MARCH JUNE SEPTEMBER
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DRIFT ACCEPTANCE +/- 5% COMMENTS: QUARTERLY CLEANINGS: MARCH JUNE SEPTEMBER
DRIFT ACCEPTANCE +/- 5% COMMENTS: QUARTERLY CLEANINGS: MARCH JUNE SEPTEMBER



Policy Number: OM 3-07N

Effective Date: 9/03

LIME BLOWERS

I. PURPOSE

Provide a consistent and reliable procedure for the Lime Blowers.

II. SCOPE

Continuous Monitoring Systems

III. RESPONSIBILLITIES

I & E Department

IV. PROCEDURE

MONTHLY

- 1. The Lime Blowers will be visually inspected each month.
 - a. Visually inspect each blower for any signs of physical damage and/or deterioration.
 Record any comments on calibration sheet.
 - b. Record flow meter reading on calibration sheet.

INSTRUMENT CALIBRATION DATA SHEET

NAME: VORTEX FLOW METER #1	
MFG: YOKOGAWA	FLOW METER READING:
MODEL#: DY	VISUAL INSPECTION:
SERIAL#: 3353B033 2003	DATE:
TAG#: VF-101	
LOCATION: LIME SILO	
NAME: VORTEX FLOW METER #2	
MFG: YOKOGAWA	FLOW METER READING:
MODEL#: DY	VISUAL INSPECTION:
SERIAL#: 3353B034 2003	DATE:
TAG#: VF-102	
LOCATION: LIME SILO	
NAME: VORTEX FLOW METER #3	
MFG: YOKOGAWA	FLOW METER READING:
MODEL#: DY	VISUAL INSPECTION:
SERIAL#: 3353B031 2003	DATE:
TAG#: VF-103	
LOCATION: LIME SILO	
COMMENTS:	
·	



Policy Number: OM 3-08

Effective Date: 9/03

CRITICAL SPARE PARTS

I. PURPOSE

Provide a list of critical spare parts.

II. SCOPE

Critical Spare Parts List

III. RESONSIBILITIES

Instrumentation and Electrical Department

IV. REFERENCES

Refer to attachments OM 3-04C and OM 3-04D.



Policy Number: OM 3-09

Effective Date: 9/03

INSPECTION SCHEDULE

I. PURPOSE

Provide a table that indicates the inspection frequencies of air pollution control (APC) equipment and continuous emissions monitoring (CEM) equipment.

II. SCOPE

APC and CEM equipment

III. RESONSIBILITIES

Kiln Operations and Instrumentation and Electrical Department

IV. PROCEDURES

Below is a table that summarizes the inspection frequencies of the air pollution control (APC) equipment and continuous emissions monitoring (CEM) equipment.

Name Inspection Frequency

Baghouse Systems	Inspected twice per shift (four inspections/24hrs.)					
Multiclones	Inspected twice per shift (four inspections/24hrs.)					
Lime Feeders and Blowers	Once per shift.					
Scrubber Systems	Once per shift					
Soda Ash Bailding	Once per shift					
Heat Exchanger and Primary Air Fans	Once per shift					
Raw Shale Belts	Once per shift					
Air Compressors	Once per shift					
Fuel Farm	Daily					
CEM/CMS equipment	Each time instruments are calibrated, they are also inspected. The calibration frequency is located in OM 3-04A. Inspection also occurs during Kiln Shutdowns.					

NORLITE CAL. SHEET CHECK LIST KILN 1

NEICVP*				
CALIBRATION TITLE	TAG#	INSTRUMENT TITLE	CALIBRATION FREQUENCY	$\frac{1}{1}$ NSTRUMENT ACCURACY ²
BAGHOUSE INLET TEMP	TT-4302	ROSEMOUNT 3044C	Monthly	+/- 0.18 F
BLOWDOWN FLOW	FT-1508	FISCHER PORTER 10D1475	Monthly	+/- 0.5% of flow rate
KILN EXIT TEMP	TT-4303	ROSEMOUNT 3044C	Monthly	+/- 0.18 F
HOOD PRESSURE D/P	DPT-5203	ROSEMOUNT 1151 DP	Monthly	+/- 0.1
I.D. FAN CURRENT	IDF-4301	ABB (ACS 600)	Monthly	± 1.0% of range
LGF FEED RATE	MM-4301	MICROMOTION DL100	Monthly	+/- 0.15% of flow rate
SCRUBBER pH A	4401A	ROSEMOUNT 2081 pH	Daily	+/- 0.02 pH
SCRUBBER pH B	4401B	ROSEMOUNT 2081 pH	Daily	+/- 0.02 pH
SCRUBBER RECIRC FLOW A	FT-4403A	FISCHER PORTER 10D1475	Monthly	+/- 0.5% of flow rate
SCRUBBER RECIRC FLOW B	FT-4403B	FISCHER PORTER 10D1475	Monthly	+/- 0.5% of flow rate
ŠHALE FEED	AR-4301	ACCURATE MPC200	Monthly	± 0.25–1.0% of rate
VENTURI D/P	DPT-4401	ROSEMOUNT 1151 DP	Monthly	+/- 0.1
SCRUBBER TANK LIQUID LEVEL	LT_101	Rosemount 1151 DP	Monthly	+/- 0.1
DRY SORBENT FEED RATE	Lime_Feed	ACCURATE 602M	Monthly	+/- 2%
DRY SORBENT CARRIER FLOW RATE	Lime_Flow	Yokogawa Model DYA-S1	MONTHLY ¹	na

na-not applicable

¹-Based on manufactures recommendation, no calibration is needed, but an inspection is conducted.

²-Based on manufactures literature.

NORLITE CAL. SHEET CHECK LIST KILN 2

20					
)E01	a itit MOITAGAI IAO	# C V F			INSTRUMENT
	CALIBRATION TITLE	#D4-	INSTRUMENT TILE	CALIBRATION FREQUENCY	$ACCURACY^2$
	BAGHOUSE INLET TEMP	TT-2404	ROSEMOUNT 3044C	Monthly	+/- 0.18 F
	BLOWDOWN FLOW	FT-2508	FISCHER PORTER 10D1475	Monthly	+/- 0.5% of flow rate
	KILN EXIT TEMP	TT-2105	ROSEMOUNT 3044C	Monthly	+/- 0.18 F
	HOOD PRESSURE D/P	DPT-2104	ROSEMOUNT 1151 DP	Monthly	+/- 0.1
	I.D. FAN CURRENT	IDF-2401	ABB (ACS 600)	Monthly	± 1.0% of range
	LGF FEED RATE	MM-2401	MICROMOTION DL100S223SU	Monthly	+/- 0.15% of flow rate
	SCRUBBER pH A	2509A	ROSEMOUNT 2081 pH	Daily	+/- 0.02 pH
App	SCRUBBER pH B	2509B	ROSEMOUNT 2081 pH	Daily	+/- 0.02 pH
endi	SCRUBBER RECIRC FLOW A	FT-2507A	FISCHER PORTER 10D1475	Monthly	+/- 0.5% of flow rate
x CA	SCRUBBER RECIRC FLOW B	FT-2507B	FISCHER PORTER 10D1475	Monthly	+/- 0.5% of flow rate
ΑE	SHALE FEED	AR-2401	ACCURATE MPC200	Monthly	± 0.25–1.0% of rate
	VENTURI D/P	DPT-2303	ROSEMOUNT 1151 DP	Monthly	+/- 0.1
	SCRUBBER TANK LIQUID LEVEL	LT_101	Rosemount 1151 DP	Monthly	+/- 0.1
	DRY SORBENT FEED RATE	Lime_Feed	ACCURATE 602M	Monthly	+/- 2%
	DRY SORBENT CARRIER FLOW RATE	Lime_Flow	Yokogawa Model DYA-S1	MONTHLY ¹	na

na-not applicable

¹-Based on manufactures recommendation, no calibration is needed, but an inspection is conducted.

²-Based on manufactures literature

Attachm 3M 3-04A

SHEET CHECK LIST MISC.

APPROVED BY:

CALIBRATION TITLE	INSTRUMENT TITLE	SYSTEM PARAMETERS	CALIBRATION FREQUENCY
LIME FEEDERS	ACCURATE	1-500 LBS/HR	Monthly
LIME TAG# AC-101	AC-102 AC-103		
CEM	CISCO	O2 / COC / HRA	Daily
PRIMARY AIR VENT (LEL)	· MSA	20% - 30%	Monthly
O2/LEL SENSORS	MSA		Monthly
QUARTERLY CAL.	(JAN.,APRIL,JULY,OCT.)	0-25 / 0-50	Monthly
FINISH PLANT PRESSURES	DWYER	0-15 "H2O	Monthly
FIRE PUMP TEST	JOSELYN CLARK	TEST RUN	Monthly
FUEL FARM VENT (O2)	SENSIDYNE	0-10 %	Monthly
PUMP SEAL ALARM CHECK	ECHOTELL/UNITED ELECTRIC	PASS/FAIL	Monthly

Norlite C - voration

Kiln # Date:

MACT OPERATING PARAMETER LIMITS
(OPLs) OM 3-04B

Test Start: Test End:

	SIGN OFF / DATE																	
THI I I I I	SIGN OFF / DATE		-															→
	STATUS	en de la companya de	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO		Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO	Alarm OPCO WFCO
	WFCO		10.3 gpm	10.3 gpm	22.0 tph	405 amps	15.0 gpm	7.9	0.0" w.c.	100 ppm @ 7% 02		866 ºF	400 °F	2.0" w.c.	40%	175 gpm	200	150
	OPCO		10.2 gpm	10.2 gpm	21.0 tph	403 amps	15.2 gpm	8.0	-0.02" w.c.	75 ppm		871 ºF	398 °F	2.3" w.c.	42%	177 gpm	210	175
AI ARM	SETPOINT		9 gpm	mdb 6	21.0 tph	401 amps	15.5 gpm	8.0	-0.03" w.c.	mdd 09		876°F	390 °F	2.5" w.c.	45%	180 gpm	220	200
	IEK	INSIDE	MAXIMUM TOTAL WASTE (LGF) FEED RATE (hra)	MAXIMUM PUMPABLE WASTE FEED RATE (hra)	MAXIMUM SHALE FEED RATE (hra)	MAXIMUM FLUE GAS FLOW RATE (ID FAN CURRENT) (hra)	MINIMUM SCRUBBER BLOWDOWN RATE (hra)	MINIMUM SCRUBBER LIQUID pH (hra) METER: A B	KILN PRESSURE ("w.c.)	CARBON MONOXIDE - LGF (hra)	OUTSIDE	MINIMUM KILN BACK-END TEMPERATURE (hra)	MAXIMUM BAGHOUSE INLET TEMPERATURE (hra)	MINIMUM VENTURI PRESSURE DROP (hra)	SCRUBBER TANK LIQUID LEVEL (hra) (% OF TANK HEIGHT)	MINIMUM SCRUBBER RECIRCULATION RATE (hra) PUMP: A B	MINIMUM LIME FEED RATE (Ib/hr) (hra) (both WFCO keys in)	MINIMUM LIME CARRIER FLOW RATE (cfm) Feeder #

Appendix CAA E Page 98 of 106

Norlite, LLC Cohoes, New York

OM 3-04B

NORLITE CC PORATION CLEAN AIR ACT MACT WFCO/OPCO PARAMETERS SPAN LIMITS

Test Start:

Test End:

OM 3-04B

NE#CVP:1120E Date D

PARAMETER	SPAN LIMITS	оьсо	WFCO	STATUS	NORLITE SIGN OFF / DATE	NYS DEC SIGN OFF / DATE
INSIDE						
TOTAL WASTF (I GF) FFFD RATE	map 02-0	19 gpm	20 ccm	OPCO		
	0-zo gpini	nidg ei	zo gprii	WFCO		
SHALE FEED RATE	0.40 tnb	35 tnh	40 toh	ОРСО		
	7-10 tpm	100 CC	t	WFCO		
FLUE GAS FLOW RATE	0-500 amps	A75 amps	500 amae	ОРСО	The state of the s	
(ID FAN CURRENT)		n called		WFCO		
KILN 1 SCRIBBER BI OWDOWN RATE	mdg 03-0	45 gpm	50 gpm	OPCO		
	0-67 gpm	52 gpm	67 gpm	WFCO		
=	35-105	10.0	40 E	ОРСО		
66 XII METER: A B	2.5.	2.		WFCO		
AA (CAM)	0 0 40 41 0	7 0 7	0.0	OPCO		
	2:1:2			WFCO		
OUTSIDE						
MINIMIIM KII N BACK-FND TEMBERATIIRE	0.1400 °E	1300 %	1400 00	OPCO		
		- 000		WFCO		
BAGHOUSE INLET TEMPERATIIRE	3º 00-20	3° 009	700 %	оьсо		
		-		WFCO		
VENTURI PRESSURE DROP	3.5" -10" w.c.	3 8 G	10 0" w C	оьсо		
				WFCO		
SCRUBBER TANK LIQUID LEVEL	700-1	95%	7000	оьсо		
(% OF TANK HEIGHT)	201-0	2/00	-	WFCO		
=	0-250 anm	245 anm		OPCO		
PUMP: A B	111 S C 2-0	111dB C+2	mdb ocz	WFCO		
National Community (Inches)	0-500	450	200	оьсо		
Feeder#	9	9		WFCO		
자 이 LIME CARRIER FLOW RATE (cfm)	0-300	280	300	OPCO		
				WFCO		

	PHASE	3	3	3	3	3	33	3	3	3	3	3	3	3	3	3	3	3	3	3	3	3		Ţ	3	
	-						対象が対象を																			
	VOLTAGE	480	480	480	480	480	480	480	480	480	480	480	480	480	480	480	480	480	480	480	480	480		120/240 SEC	120/208 SEC	
-									· · · · · · · · · · · · · · · · · · ·									A144								
	RPM	1200	1200	1800	1800	1800	1200	1800	1800	3600	3600	1800	3600	1800	1800	1800	3600	3600	3600	1800	1200	1800/1200		480V PRI.	480V PRI.	
3/5/03									HAZ/:LOCATION						HAZ. LOCATION									OUTDOOR	INDOOR	
	FRAME	587T	449T	445T	405T	364T	365T	324T	324TCE	324TS	286TS	286T	284TS	284T	284T	254T	254T	215T	215T	215T	256T	254T	Views - da	TRANS.	TRANS.	
															新新教育											
	HP	400	200	150	100	09	20	40	40	40	30	30	25	25	25	15	15	15	10	10	10	5/2.2		25 KVA	150 KVA	
									がなる。											1						
	QTY	-	-	-	2	-	-	2	_	-	-	-	-		-	-	-	-	-	-	1	-	_	1	_	

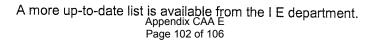
A more up-to-date list is available from the I E department.

PHASE	3	3	3	3	3	3	3		3	3	3	3			-	-	3	-	-	
	特不如不是			是 包括															:	
VOLTAGE	480	. 480	480	480	480	480	480	90VDC	480	480	480	480	90VDC	90VDC	115	115/230	480	230	115	
RPM	3600	3600	3600	1800	1800	1800	1200	1800	1200	1800	1800	1800	1800	53	1800	2900-3400	1800	1050	1700	
																	Unimount			
FRAME 213T	213T	184T	184TC	184T	145T	145TC	182T	29C	29C	29C	29C	56	26C			42CZ	B56	446		DRIVE
																	10 (10 (10 (10 (10 (10 (10 (10 (10 (10 (
HP 7.5	7.5	5	5	5	2	2	1.5	3/4	3/4	3/4	1/2	1/2	1/2	1/4	1/6	0.08	1/2	1/6	1/6	20
QTY	-	-	-	_	0	2		-	-	-	2	-	_	2	-	2	2	2	-	_

A more up-to-date list is available from the I E department.

INSTRUMENTATION SPARES

MANUFACTURER	SIZE	TYPE	QUANITY	RANGE
Fischer Porter	4"	Flow	3	
Fischer Porter	1 1/2"	Flow	3	
Fischer Porter	1"	Flow	3	
Rosemount		Pressure	2	0 - 10" H ₂ 0
Rosemount		Pressure	2	0 - 15" H ₂ 0
Rosemount		Pressure	2	0 - 200 psi
Rosemount		Pressure	1	0 - 60" H ₂ 0
Rosemount		Pressure	1	0 - 6" H ₂ 0
Rosemount	· · · · · · · · · · · · · · · · · · ·	Pressure	1	0 - 110" psi
Rosemount		Pressure	1	(-)2.0 - 1.0" H ₂ 0
Rosemount		Pressure	2	0 - 20 psi
Rosemount		Temperature	5	0 - 100°c
Worcester	***************************************	Valve Actuator	2	Series 75
Worcester		Valve Actuator	2	Series 75
Sensorex	The state of the s	Ph probe	10	S660CD
Dwyer		Photohelic	3	
CEM Equipment		Regulator	4	· · · · · · · · · · · · · · · · · · ·
CEM Equipment		Stone Filter/Gaskets	10	
CEM Equipment		Paper Filters	10	**************************************
CEM Equipment		Vacuum Pump	3	
CEM Equipment		Perma Pure Filter	2	
BHA CPM 750		Bag Leak Detector	1	0-100%





Policy Number: OM 4-01

Effective Date: 9/03

CONTINUOUS MONITORING SYSTEM

PURPOSE I.

Provide a procedure to ensure the correct operation of the Continuous Monitoring System (CMS).

II. **SCOPE**

CMS

III. RESPONSIBILLITIES

Instrumentation and Electrical Personnel (I & E)

IV. **PROCEDURES**

The CMS runs continuous for 24 hours a day, seven days a week and 365 days a year. Therefore, the main function is to keep the CMS calibrated and provide routine maintenance of the system. The following describes how the CMS is maintained on a daily basis.

- Daily calibrations for the Continuous Emissions Monitoring (CEM) system are done 1. on Kiln 1 (Train A and Train B) and Kiln 2 (Train A and Train B) to ensure correct reporting of data. See OM 4-01A for a copy of the CEM Daily QA/QC log sheet. The system is inspected each day to ensure correct data reporting, if maintenance of the system is required, it will be performed at that time.
- Calibrations and maintenance are performed on non-CEM CMS as described in OM 2. 3-06. The frequency these instruments are calibrated is located in OM 3-04A. The forms used to record the calibrations are OM 4-02A thru OM 4-02O.
- Besides the Instrumentation and Electrical (I&E) department performing calibrations, 3. the kiln control room operator is continually monitoring all instrument outputs. If a discrepancy in noticed with the instruments, I&E is called upon to check the instrument reading.
- Should a problem develop within the workstation, PLC or DAS; contact I&E to look 4. into the situation.

The only exception when the CMS system is shutdown is when a programming change to the PCL and DAS is needed. This would only occur when the kiln is not operating on hazardous fuels.

Norlite Corporation

Laboratory Fuel Blending & Certification Guidelines

SOP#04-042 Revision #1

> Date Prepared: 09/08/03 Prepare by: Prince Knight

Approved by:

Document Letter:__

1.0 Scope

The following procedures will provide guidelines for the tracking, blending and certification of Low Grade Fuel received into Norlite. Due to the presence of many variables, the following SOP will only act as a guideline and operational managers should be consulted for final decisions and certification.

2.0 References

Norlite Corporation's Hazardous Waste Management Permit under Article 27, Title 9; 6NYCRR 373. Norlite Analytical Laboratory's Quality Manual NYS DOH ELAP Manual NELAC Manual Chapter 5.0 "Quality System" Various Computer Program Manuals; See specific sections for any detailed references.

3.0 Safety

There are no special safety requirements required for this SOP.

4.0 Process / Required Materials / Software Programs

- -Corel Quattro Pro
- -Microsoft Excel
- -Borland Q&A Report Writer (Database)
- -BackupExec Tape Drive system
- -Fuel Farm Blending and Tank Transfer sheet
- -Norlite Laboratory analytical results (or other NYS DOH ELAP certified results)

5.0 Processes

5.1 LGF Tracking and Updating

- 1. Identify the LGF shipment to be tracked. Locate the certified analytical results and the Fuel Farm Tracking sheet with the entry that contains the off loading or transfer information.
- 2. Open the Corel Quattro Pro spreadsheet program to the file which contains the analytical information of the receiving tank.
- 3. Any existing material in the tank must be accounted for by using the "current" chemistry as the new starting chemistry of the tank with the associated gallons that were in the tank before the LGF material was off-loaded / transferred. This will ensure not only accurate tank analytical, but will also provide tracking and contact information for all future materials added to the tank.
- 4. Add a new column of chemistry by adding the analytical information associated with the LGF material obtained from the certified analytical results. Determine the volume, in gallons, of the material added to the tank using one of the following methods:
 - -Certified weight ticket converted to gallons using the material's specific gravity.
 - -Fuel Farm PLC gauge readings of the receiving tank
 - Manifested information provided by the generator.
 - -Any combination of the previous three if there is an error or malfunction that affects the volume calculation.
- 5. The tank spreadsheet will automatically calculate the final chemistry by computing the mass weighted average of each LGF entry and the starting chemistry of the tank. The final resulting chemistry will be displayed in the furthest right hand column labeled "Finish".
- 6. The Data Checking System (DCS) value at the bottom of each column entry must be compared to the DCS value located on the analytical results sheet. The DCS value should match to ensure no data entry errors have occurred. The DCS values of the Finish column and overall DCS value should also be compared to ensure no computational errors have occurred.
- 7. A new tank status sheet can be updated a this time by opening a daily tank status sheet which directly references the data cells of each individual tank. The program automatically updates the analytical information for each tank and only the tank levels require manual input based on the Fuel Farm transfer sheet documented gauge readings.

5.2 LGF Blending

- 1. Using a current tank status sheet, qualified laboratory or fuel farm personnel can forecast blends using the Corel Quattro Pro Program. By adjusting the levels of each tank accordingly, a theoretical blend can be projected by using the same mass weighted average calculation as the individual tank updates.
- 2. Forecasted blends should be based on facility operational issues such as metals and chlorine dilution, BTU heat value optimization, special handling waste streams and tank volumes.
- 3. A theoretical blend should be tested by inserting the projected analytical chemistry into a test Waste Analysis Plan (WAP) 2 sheet. (See LGF Certification 5.3) The DCS values listed on the theoretical blend should match the DCS on the WAP-2 sheet to verify no data entry errors have occurred. If the projected blend is "certifiable" using maximum LGF (10.1 gal/min) and the maximum heat value (62,000,000 BTU/hr) The blend may be given to the fuel farm. If the blend cannot be maximized in this way, either adjust the tank levels to ensure a certified blend, or obtain management direction to proceed with a "restricted" blend.
- 4. Provide the final theoretical blend to the fuel farm representative. Maintain a copy of the blend at the laboratory for further comparisons. When the fuel farm operators have finished the blend, obtain a copy of the Fuel Farm Transfer Sheet and locate the blend information.

5.3 LGF Certification

- 1. Update the receiving tank as indicated in section 5.1 of this SOP. Verify that the final DCS value compares to the DCS value located on the theoretical blend sheet. This not only ensures no data entry errors have occurred, but also that the blend was completed as intended.
- 2. Review the final tank chemistry and compare to permitted values located on the right hand side of the spread sheet. If any value falls outside of permit compliance, seek management input for re-blending or certification options. If there are no issues, assign the tank a WAP-2 sequential file number and update the tank sheet accordingly. Record the file number in the WAP-2 log book. Print both this file raw data sheet and the associated Kiln Oil tank sheet for permanent documentation.
- 3. Issue an official WAP-2 sheet for each Kiln by updating the information in the Borland Q&A Database program. Maximize the BTU/hr value by incrementally adjusting the Kiln Oil gal/min value and recalculating the WAP-2 sheet. Once the WAP-2 sheet is finalized, print a copy for each kiln and keep together with the raw data sheets.
- 4. Two, qualified laboratory personnel must review the WAP-2 sheet and compare at minimum, the following; File#, Tank identification, certified volume, DCS comparison, LGF rate, Kiln Oil rate, BTU/hr, Date released, tank contents and BTU/pound and specific gravity of the LGF. If all values check with the raw data sheets which have been checked versus the projected blend, the laboratory personnel may sign the WAP-2 sheet as certified and deliver to the Kiln operators for operational instructions.

6.0 Record Keeping

- 1. All original WAP-2 sheets must be returned from the kiln for monthly facility reporting and final storage in Norlite's Document Control System.
- 2. All computer data relating to tank spreadsheets and tank status sheets are organized and backed up on a daily basis. This is completed by running a back up macro in Quattro Pro and saving the file as the date. Furthermore, all sheets and Q&A database files are backed up daily and weekly using a tape drive back up system. Electronic storage media are stored in a locked, fireproof safe.
- 3. Fuel farm off-loading and transfer sheets are maintained as part of a daily packet which includes tank status sheets, projected blends and any other operational documentation needed to recreate the LGF activities of that day.
- 4. Original analytical data packets, generated by the laboratory are kept on file as computer database files and hard copy records. The data packets will contain the minimum information to reference all raw data results.